

1 **Performance of full-scale rural wastewater treatment plants in the reduction of antibiotic-resistant**
2 **bacteria and antibiotic resistance genes from small-city effluents**

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19 **Abstract**

20 The main objective of this study was to evaluate the performance of full-scale rural wastewater treatment
21 plants (WWTPs) in the reduction of antibiotic-resistant bacteria (ARB) and antibiotic resistance genes
22 (ARGs) from small-city effluents. Twenty full-scale WWTPs in rural Chile with different biological
23 treatment technologies (vermifiltration (VF), activated sludge (AS) and biodisc (BD)) and disinfection
24 treatments (chlorination (Cl) and UV irradiation (UV)) were monitored and studied in two campaigns:
25 Campaign 1 (20 WWTPs) and Campaign 2 (6 WWTPs). In both campaigns, the rural WWTPs improved
26 the water quality of the effluents very significantly (90%, 70%, and 40% reductions in TU, COD, and NH_4^+ -
27 N, respectively) and reduced ARB and ARG loads by 2 to 4 log units. All three biological treatments
28 contributed to the final quality of the effluents, especially in terms of microbiological parameters, with
29 statistically indistinguishable efficiencies between them. These results show the importance of rural
30 WWTPs in improving the water quality of urban effluents while reducing microbiological risk and the
31 spread of antibiotic resistance into the environment. The study demonstrates the utility of a non-centralized,
32 self-managed wastewater treatment scheme that can be implemented in many sparsely populated areas
33 around the world.

34 **Keywords:** antibiotic-resistant bacteria; antibiotic resistance genes; biological treatment; water quality
35 parameters, principal component analysis, disinfection

36

37 **1. Introduction**

38 Wastewater treatment plants (WWTPs) have a significant role in the spread of resistance among the bacteria
39 into the environment [1–2]. On the one hand, WWTPs contribute greatly to the protection of public health
40 and the aquatic environment by reducing the transmission of waterborne diseases and aquatic pollution [3].
41 On the other hand, the presence of diverse selection pressures, such as high antibiotic concentrations, and
42 microbial growth conditions in WWTPs create a favorable environment for the transfer of antibiotic
43 resistance genes (ARGs) and the proliferation of antibiotic-resistant bacteria (ARB) [4].

44 The performance of urban WWTPs has been widely investigated, with reported ARB and ARG reductions
45 varying between 1.0 – 4.0 log units relative to the untreated inputs [5–7]; however, fewer studies have
46 focused on evaluating the performance of rural WWTPs. In general, the chemical oxygen demand (COD)
47 and ammonium nitrogen ($\text{NH}_4^+\text{-N}$) removal efficiencies in those systems varied between 30 – 860 $\text{g/m}^3\cdot\text{d}$
48 and between 10 – 140 $\text{g/ m}^3\cdot\text{d}$, respectively [3]. In the case of ARB and ARGs, the reported reductions lie
49 within the 1 – 3.0 log units range [8]. This information is significant for developing countries like Chile,
50 where 12% of the population resides in rural areas, which have only 20% wastewater treatment coverage
51 [9,10]. In this context, access to water and sanitation in Chilean rural areas is facilitated through small
52 committees, in which residents manage and operate small drinking water and wastewater treatment
53 facilities. These organizations, known as “Rural Sanitary Services,” aim to provide water and treatment to
54 concentrated and semi-concentrated rural populations ranging from 80 to 3000 inhabitants [11]. Among the
55 available biological wastewater treatment technologies, activated sludge treatment (AS) is the most
56 employed for rural WWTPs, although vermifiltration (VF) and biodisc (BD) systems are also commonly
57 used [10]. Both AS and BD involve aerobic treatment, with the difference being that BD uses rotating discs
58 to develop a biofilm capable of degrading organic matter, while AS consists of an aeration tank where a
59 flocculent culture of microorganisms is developed [12,13]. In the case of VF, this promising treatment is
60 composed of earthworms and compost bedding, in which earthworms are responsible for degrading organic

61 matter and nutrients [14]. Although these technologies were not designed to remove ARB and ARGs, it has
62 been proposed that treatment processes can reduce ARB and ARGs loads, avoiding microbiological risks to
63 the environment and human health [4].

64 The influence of different wastewater technologies on ARG and ARB removal has been studied to a limited
65 extent. Many studies have revealed that the removal of ARGs and ARB in wastewater is influenced by
66 technology type, operational and design parameters, and disinfection treatment [1,4,15,16]. The efficiency
67 of these technologies in reducing ARB and ARG loads has been extensively reported for AS, but there are
68 few comparable studies for BD and VF. The efficiencies of the three treatments appear to be very similar,
69 with reduction between 1.8 – 2.6 log units for ARBs and 1.1 – 4.1 log units for ARGs in the case of AS [6],
70 and between 2.0 – 4.0 log units for BD and VF [17,18]. Regarding disinfection processes, Zhuang et al. [19]
71 and Zheng et al. [20] investigated the efficiency on ARG removal using chlorination (Cl), ultraviolet
72 irradiation (UV), and ozonation (O₃) disinfection in WWTPs. In both cases, disinfection by Cl presented
73 better performances, with reduction values above 3.0 log units.

74 Against this backdrop, the present study is among the first to analyze the contribution of rural WWTPs to
75 the spread of antimicrobial resistance (AMR), examining the difference between biological and disinfection
76 technologies. Thus, the main objective of this study was to evaluate the performance of full-scale rural
77 wastewater treatment plants in the reduction of ARB and ARGs, analyzing twenty WWTPs in rural Chile
78 that use various biological wastewater treatment technologies (VF, AS, BD) and disinfection processes (Cl
79 and UV).

80 **2. Material and Methods**

81 **2.1 Sample collection from rural wastewater treatment plants**

82 This study was conducted in two sample-collection campaigns (Campaign 1 and Campaign 2) at twenty
83 full-scale rural WWTPs located in the Biobio Region, Chile (36°46'22"S 73°03'47"W, Figure S1 in the

84 supplementary information). Figure 1 shows the sampling map, displaying the locations of the WWTPs and
85 their corresponding biological treatments. The selected WWTPs serve areas with populations that vary
86 between 88 and 2533 inhabitants (Table S1 in the supplementary information). During Campaign 1, the
87 twenty full-scale rural WWTPs were studied and monitored, with physicochemical and microbiological
88 parameters and ARB abundances analyzed. After the initial screening in Campaign 1, two plants per
89 biological treatment technology (VF, AS, BD) were resampled, resulting in a total of six WWTPs monitored
90 during Campaign 2. The criteria used to select these WWTPs were geographic proximity to the laboratories
91 and operating efficiencies (data not shown). In Figure 1, these WWTPs were highlighted in red. In addition
92 to the analysis carried out in campaign 2, ARG abundances were determined.

93 *Figure 1*

94 **2.1.1. Campaign 1**

95 Figure 2 shows a schematic diagram of different biological and disinfection treatment technologies. In
96 Campaign 1, four, nine, and seven rural WWTPs with AS, BD, and VF biological treatment technologies,
97 respectively, were analyzed. Each plant used a primary treatment of grids and sieves, followed by a
98 secondary treatment involving a biological technology (VF, BD, or AS), and finally a Cl or UV disinfection
99 treatment process. For each WWTP, samples were collected at three monitoring points: influent (after the
100 primary treatment) (I), secondary effluent (SE), and final effluent (FE) (Fig 2). The sampling was conducted
101 at a single point per plant from September 2021 to November 2021. Samples were stored in amber bottles
102 at 4 °C and processed within 48 h.

103 *Figure 2*

104 **2.1.2. Campaign 2**

105 Six full-scale rural WWTPs were selected from Campaign 1 using the specific biological treatment as a
106 selection criterion. For VF technology, the selected WWTPs were Copiulemu (VF1, 36° 53' 25.474" S and

107 72° 48' 26.64" W) and Villa Las Almendras (VF3, 37° 16' 51.715" S and 72° 38' 25.221" W). Both plants
108 use a primary treatment of grids and sieves followed by a secondary treatment using VF technologies.
109 Regarding disinfection, VF1 employed UV irradiation, while VF3 used a Cl process. For AS technologies,
110 both plants use a primary treatment with grids and sieves followed by a secondary AS treatment. These
111 plants employed Cl as a disinfection process. The WWTPs selected were Rere (AS1, 37° 7' 52.19" S and
112 72° 43' 37.653" W) and Río Claro (AS2, 37° 12' 17.029" S and 72° 37' 9.583" W). The selected BD systems
113 have the same treatment train as the VF systems, using different disinfection processes. In the case of Villa
114 Laja (BD1, 37° 15' 23.321" S and 72° 41' 30.14" W), the disinfection process used was UV irradiation,
115 whereas Santa Fe (BD2, 37° 28' 22.733" S and 72° 34' 35.696" W) used Cl as a disinfection technology.
116 Water samples were collected as in Campaign 1 (I, SE, and FE), with the sampling performed at fixed points
117 in each plant between May 2022 and June 2022 (Fig.2). Water samples were stored in amber bottles at 4 °C
118 and processed within 48 h after sampling.

119 *Figure 2*

120 **2.2. Physicochemical characterization of water samples**

121 Physicochemical characterization of water samples was carried out during both Campaign 1 and Campaign
122 2. The I, SE, and FE samples from each WWTP were filtered using a 0.45- μ m-pore-size Whatman
123 membrane. The in-situ parameters such as pH, temperature (°C), electrical conductivity (EC), and oxidation-
124 reduction potential (redox) were measured using OAKTON portable equipment (PC650-480485,
125 OAKTON, USA). Dissolved oxygen (DO) concentration and turbidity (TU) were determined using a
126 portable oxygen sensor (HANNA OXI 330i/set HI 9146-04, HANNA Instruments Inc., USA) and a portable
127 waterproof turbidimeter (OAKTON T-100, OAKTON, USA), respectively. The concentrations of COD
128 (colorimetric method), NH_4^+ -N (colorimetric method at 640 nm), nitrate nitrogen (NO_3^- -N, colorimetric
129 method at 220 nm and 275 nm), nitrite nitrogen (NO_2^- -N, colorimetric method at 543 nm), and phosphate
130 phosphorus (PO_4^{3-} -P, colorimetric method at 890 nm) were measured based on the protocols described in

131 Standard Methods [21]. In the case of microbiological parameters, total coliforms (TC) and fecal coliforms
132 (FC) were counted by serial filtration of water samples (I, SE, EF) in nitrocellulose with a 0.45 µm pore
133 size. The membrane filters were placed on chromogenic selective agar (Chromocult ® Coliform Agar ES,
134 Merck) and incubated at 36 °C for 24 h. The filters with countable salmon-red colonies (TC) and dark blue
135 to violet colonies (FC) were selected.

136 **2.3. Determination of antibiotic-resistant bacteria (ARB) in water samples**

137 ARB abundances were determined in water samples (I, SE, EF) during Campaign 1 and Campaign 2. The
138 plate count technique based on the ability of bacteria to grow in the presence of an antibiotic was used to
139 measure the ARB abundances, expressed in colony-forming units (CFU)/100 mL. The I, SE, and FE water
140 samples from each WWTP were incubated at 30 °C for 24 h using MacConckey agar as a culture medium;
141 this is a selective medium for Gram-negative bacteria. The plates were supplemented with commonly used
142 antibiotics in Chile, such as ciprofloxacin (CIP), amoxicillin (AMX), and ceftriaxone (CTX) (OXOID,
143 Thermo Scientific), at concentrations of 2 mg/L, 32 mg/L, and 4 mg/L. These concentrations represent the
144 breakpoint values for defining resistance to these antimicrobial agents [22]. For the spread of plate method,
145 different water dilutions were used depending on the water samples. In the case of I, SE and FE, the water
146 dilutions were from 10⁻⁵ to 10⁻², from 10⁻⁴ to 10⁻¹ and from 10⁻³ to samples without dilutions, respectively.
147 Only plates with 30 to 300 colonies were used for enumeration.

148 **2.4. Quantification of ARGs**

149 **2.4.1. DNA extraction from water samples**

150 DNA extraction and ARG quantification were carried out only for water samples (I, SE, FE) from the
151 WWTPs selected for Campaign 2 analysis (VF1, VF3, AS1, AS2, BD1, and BD2). Water volumes of 0.5
152 L, 0.5 L, and 1 L for I, SE, and FE samples, respectively, were filtered through a membrane with 3.0-µm
153 (Polycarbonate membrane filter, Millipore, Merck, USA) and 0.2-µm pore sizes (Polytetrafluoroethylene

154 (PTFE) membrane filter, Omnipore, Merck, USA) and stored at -20°C until further use. DNA was extracted
155 using Qiagen DNeasy Power Soil kit (Qiagen, Inc., Valencia, CA) to a final elution volume of 50 µL from
156 the different membrane used (3.0-µm and 0.2-µm pore sizes). The concentration and the quality of the DNA
157 were tested using a Nanodrop Spectrophotometer 8000 (Thermofisher Scientific, Inc., Waltham, MA). The
158 extracted DNA from the water samples from each WWTP was stored at -20°C until further use.

159 **2.4.2. qPCR**

160 Five ARGs of interest were selected and analyzed in water samples from each WWTP during Campaign 2:
161 *sul1*, *bla_{TEM}*, *qnrS*, *bla_{CTX-M-32}*, and *tetM*, as well as 16S rDNA and *intI1*. ARGs were quantified using SYBR
162 green (A F. Hoffmann–La Roche AG, Inc, Switzerland), except for *tetM*, for which Dynamo ColorFlash
163 SYBR green was used (Thermofisher Scientific, Inc.), in a Lightcycler 480 (A F. Hoffmann–La Roche AG,
164 Inc, Switzerland). The thermal cycling conditions were 95 °C for 10 min, 45 cycles at 95 °C for 15 s, and
165 Ta for 1 min. The quantitative PCR (qPCR) reactions were performed in duplicate using fixed dilution of
166 raw DNA extract. The quality criterion was $R^2 > 0.99$. The ARG quantification was based on the protocols
167 described by Cerqueira et al. [23].

168 **2.5. Statistical analyses**

169 In this study, the performance of full-scale rural WWTPs in ARB, ARG, TC, and FC reductions and
170 physicochemical parameters among different biological treatments and disinfection treatments during
171 Campaign 1 and Campaign 2 was analyzed using RStudio version 4.3.1, with a significance level of $p =$
172 0.05. The data were tested for normality and homogeneity of variance using the Shapiro Wills test and
173 Fligner-Killen test, respectively. Then, an ANOVA test for the data with a normal distribution and a
174 Kruskal-Wallis test for the data without a normal distribution were performed. In this case, comparison
175 between I, SE, and FE and the effect of WWTP characteristics was carried out by means of the Kruskal-
176 Wallis test and Dunnet post-hoc test using the `Dunn.test` R package (<https://cran.r->

177 project.org/web/packages/dunn.test/index.html). The effects of biological technologies and disinfection
178 processes were studied by means of a two-way Permanova test using the vegan R package ([https://cran.r-](https://cran.r-project.org/web/packages/vegan/index.html)
179 [project.org/web/packages/vegan/index.html](https://cran.r-project.org/web/packages/vegan/index.html)). Finally, PCA was performed using the principal function from
180 the psych R package (<https://cran.r-project.org/web/packages/psych/index.html>).

181 **3. Results and discussion**

182 **3.1. Influence of full-scale rural WWTPs on physicochemical and microbiological parameters** 183 **(Campaign 1)**

184 The efficiency of the studied WWTPs in removing nutrients and microbiological (including ARB) loads is
185 presented in Table 1. The physicochemical analysis of influents (I, Table 1) allows them to be classified as
186 concentrated, according to Henze et al. [24] (COD > 300 mg/L, NH₄⁺-N > 50 mg/L and FC > 8.0 log
187 (CFU/100 mL) (Table 1). WWTP treatment reduced TU, COD, and NH₄⁺-N loads by 92%, 79%, and 53%,
188 respectively (Table 1, all WWTP combined). Primary and secondary treatments accounted for essentially
189 all (COD and NH₄⁺-N) or most (TU) of the observed load reduction, suggesting that the tertiary disinfection
190 treatments made a moderate contribution to the quality of the final effluent, at least in terms of
191 physicochemical parameters (Table 1). These performance levels were in the ranges reported in previous
192 analyses of WWTPs equipped with similar biological tertiary treatments [17,25,26].

193 *Table 1*

194 WWTP treatment also very significantly reduced the overall microbiological loads (Table 1). TC and FC
195 counts were reduced by 3.1 – 3.8 log units and 2.4 – 2.7 log units, respectively, with no significant
196 differences among the three biological treatments ($p > 0.05$, Table 5S). A similar tendency was observed
197 for the reduction of CIP-, AMX- and CTX-resistant bacterial loads (ARB^{CIP}, ARB^{AMX} and ARB^{CTX},
198 respectively, Table 1). In this case, the tertiary treatment reduced TC, FC, and ARB^{CIP} loads relative to the
199 secondary effluent, demonstrating its utility for removing potentially pathogenic microorganisms and
200 reducing AMR spread into the environment (Table 1). These findings are consistent with those of Zhuang

201 et al. [19], who studied the effects of Cl, UV, and O₃ on ARB and ARG reductions, reporting an ARB
202 reduction of 3 – 4 log units from SE to FE; however, no significant differences in overall performance were
203 observed among the three biological (VF, AS, and BD, Table 5S) and disinfection treatments. These
204 performances in coliform and ARB load reduction are similar to those found in the literature, which ranged
205 between 2 and 4 log units [27,28]. They also compared well with those obtained using more sophisticated,
206 more energy- and resource-intensive, and potentially more aggressive secondary treatments, like the
207 oxidation ditch (OD) or a membrane biological reactor (MBR) [18]. These results show that the full-scale
208 rural WWTPs of this study decreased the environmental risks of the FE in terms of eutrophication regardless
209 of the type of biological technology.

210 The mutual correlations among the 60 water samples analyzed in this work (three samples (I, SE, and FE)
211 each from each 20 WWTPs) according to their physicochemical and microbiological characteristics were
212 analyzed using PCA (two components, 47% of total variance explained, Figure 3). The score plot (Figure
213 3a) shows input (I) samples neatly separated from the treated (SE and FE) ones, consistent with the
214 characteristics of the influent and the observed effect of the treatment on the studied parameters. The same
215 plot shows much less separation between secondary and final effluent samples, also in agreement with the
216 results of the global analyses (see Table 1). It also shows no differences among the three biological and
217 disinfection treatments, as FE samples from WWTPs equipped with all three methods are clustered together
218 in the graph (Figure 3a, see green circles, diamonds, and triangles). Comparison of the loading plot with the
219 score plot (Figure 3b) indicates that influent samples are associated with high loads COD, TU, NH₄⁺-N,
220 microbial parameters (TC and FC), and ARB abundances (ARB^{CIP}, ARB^{AMX} and ARB^{CTX}), which is
221 expected due to the characteristics of the input wastewater and the reduction of these loads due to the
222 secondary and tertiary treatments (Table 1). Therefore, this multivariate parametric analysis reflected the
223 global results, indicating that most of the depuration effects corresponded to the primary and secondary
224 WWTP treatments (SE), whereas the tertiary disinfection treatment contributed a minor refinement,

225 although it was likely significant for the improvement of the microbiological parameters. The relative
226 performance of the different steps of the water treatment may be attributed to the fact that the biological
227 treatments used in this study were aerobic.

228 *Figure 3*

229 **3.2. ARG removal and its relationship to physicochemical and microbiological water quality** 230 **parameters (Campaign 2)**

231 Physicochemical and microbiological parameters of the water samples collected in the six selected WWTPs
232 for resampling in Campaign 2 presented TU, COD, $\text{NH}_4^+\text{-N}$, TC, and ARB removal efficiencies similar to
233 the results from Campaign 1 (Table 2, compared with Table 1) despite the smaller sample size, the six
234 months between the two campaigns, and the subsequent change in season (spring for Campaign 1, fall for
235 Campaign 2). In addition, analysis by qPCR of absolute abundances of 16S rDNA, *intI1*, and the ARGs
236 *sul1*, *bla_{TEM}*, *qnrS*, *bla_{CTX-M-32}*, and *tetM* showed a very effective removal of these DNA sequences from the
237 final effluent relative to the input, with levels in some cases falling to below quantitation limits (Table 2).
238 As in Campaign 1, most of the reduction in nutrient and microbiological loads occurred during secondary
239 treatment, although the tertiary treatment provided a further reduction in several parameters, particularly
240 TC, *intI1*, *bla_{CTX-M-32}*, and *tetM* (Table 2). Munir et al. [18] observed little change in ARG and ARB
241 abundances between pre- and post-disinfected effluents. As in the case of Campaign 1, no differences were
242 observed among the three biological treatments and disinfection processes (Cl vs. UV) (Figure 5, see also
243 supplementary Table 7S), although the statistical tests may be hampered by the relatively small amount of
244 samples (only two samples per biological treatment class). Figure 4 shows the distribution of samples taken
245 during Campaign 2 (PCA, two components, 67% of total variance explained). The plots show a strong
246 similarity to their counterparts for Campaign 1 (Figure 3), although the separation between SE and FE
247 samples in the score plot (Figure 4a) is clearly better defined in the Campaign 2 analysis. The loading plot
248 in Fig. 4b suggests a strong co-correlation between microbiological parameters (TC, FC), ARB (ARB^{CIP},

249 ARB^{AMX}, ARB^{CTX}) and ARGs. This tendency was also reported by Kumar et al. [29] who evaluated the
250 prevalence of ARB and ARGs in two municipal WWTPs and one hospital WWTP and found a strong
251 association between coliform prevalence and ARB abundance. In the same line, Narciso-da-Rocha et al.
252 [30] reported that ARGs such as *bla*_{TEM} and *vanA* presented a strong correlation with culturable-bacteria,
253 antimicrobial residues, and some bacterial populations. These associations between microbiological (TC
254 and FC) and AMR parameters (ARB and ARGs) are relevant for monitoring the risks of AMR dissemination
255 into the environment in rural WWTPs. While a molecular technique like quantitative PCR (qPCR) is a useful
256 and easy-to-use tool for the direct determination of ARGs, the application of such techniques in rural
257 WWTPs is difficult in terms of the need for sophisticated equipment and highly trained personnel. For this
258 reason, TC and FC could be a useful indicator of reductions in microbiological and AMR parameters in
259 rural WWTPs [6].

260 *Figure 4*

261 In general, the most abundant ARGs in the input samples were *sul1* and *int11*, with values that fluctuated
262 between 5.0 – 5.5 log copies/mL (Table 2). A relationship between *sul1* and *int11* abundances was observed
263 in the literature; this tendency is expected, as *sul1* is located in the 3' conserved region of Class 1 integrons
264 [31]. This finding is consistent with Shen et al. [32] and Zhang et al. [33], who reported a correlation between
265 *sul* genes and *int11* in WWTPs in China. The reduction of over 4 log units in ARB and most ARGs loads
266 (Table 2) is similar to those found in studies on WWTPs in the literature, with values that varied between
267 2.0 – 4.5 log units [6,26,33]. Regarding the overall effect of disinfection in rural WWTPs, the results confirm
268 that the biological treatment and subsequent disinfection could play an important role in removing ARGs
269 and serve as a barrier that limits ARB and ARGs dissemination into the environment [20,34–37].

270 *Figure 4*

271 **4. Conclusions**

272 The overall results regarding the performance of rural WWTPs in both campaigns demonstrated that the
273 combination of secondary and tertiary treatments is a good design for reducing the risks of microbiological
274 and AMR dissemination and improving FE quality in rural areas where the WWTP management and
275 operation have economic and technical limitations. It is also revealing that no differences between the types
276 of biological and disinfection technologies were reported, indicating a similar efficiency for all of them, at
277 least within the limitations of our study. The overall reductions in TU, COD, and NH_4^+ -N loads were above
278 90%, 70%, and 40% in both campaigns, whereas coliform loads were reduced by between 2.0 and 4.0 log
279 units, ARB loads between 2.0 and 4.6 log units, and ARG loads between and 2.3 and 4.0 log units. These
280 results underscore the importance of these rural WWTPs in improving the water quality of effluents,
281 decreasing eutrophication, and reducing microbiological risks and the spread of AMR. The fact that these
282 results were obtained in essentially self-managed WWTPs only adds interest to a non-centralized scheme
283 of wastewater treatment that has proved very useful for sparsely populated areas around the world.

284

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296 **Authors Contributions**

297 All authors contributed to the study conception and design. Material preparation, data collection and analysis
298 were performed by Ana María Leiva and Gloria Gómez. The first draft of the manuscript was written by
299 Ana María Leiva and Gerardo González-Rocha, Benjamín Piña and Gladys Vidal corrected and commented
300 on previous versions of the manuscript. All authors read and approved the final manuscripts.

301 **Ethical approval**

302 The manuscript does not contain data which requires ethical approval.

303 **Consent to participate**

304 All the authors have consent to participate.

305 **Consent for publication**

306 All the authors have consent to publish.

307 **Competing interests**

308 The authors have no relevant financial or non-financial interests to disclose.

309

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Parameter	Unit	Overall			Final Reduction* or
		I	SE	FE	Removal
					Efficiencies** (%)
pH	-	7.5 ± 0.9	6.9 ± 0.8	6.9 ± 0.7	n/s
T	°C	19.0 ± 1.7	19.1 ± 1.9	19.2 ± 1.9	n/s
Redox	mV	54.8 ± 170.9	85.1 ± 140.2	129.5 ± 175.0	n/s
EC	µS/cm	1.0 ± 0.2	0.9 ± 0.2	0.9 ± 0.2	n/s
DO	mg/L	2.7 ± 1.8	3.2 ± 1.8	3.6 ± 2.2	n/s
TU	NTU	176.2 ± 58.5 ^A	36.5 ± 24.3 ^B	13.9 ± 12.9 ^C	92.3 ± 6.0%**
COD	mg/L	365.5 ± 213.5 ^A	88.1 ± 60.8 ^B	63.0 ± 42.0 ^B	77.2 ± 21.9%**
NH₄⁺-N	mg/L	57.2 ± 35.1 ^A	27.0 ± 15.8 ^B	24.1 ± 18.7 ^B	52.9 ± 25.2%**
NO₃⁻-N	mg/L	4.0 ± 3.0	3.4 ± 3.1	3.1 ± 3.2	n/s
NO₂⁻-N	mg/L	0.2 ± 0.3	0.2 ± 0.3	0.3 ± 0.3	n/s
PO₄²⁻-P	mg/L	10.0 ± 6.9	8.1 ± 4.0	8.1 ± 3.5	n/s

TC	log (CFU/100 mL)	8.7 ± 8.5 ^A	7.2 ± 7.5 ^B	5.8 ± 6.2 ^C	2.9 ± 1.2 logs*
FC	log CFU/100 mL	7.9 ± 8.2 ^A	6.7 ± 7.0 ^B	5.6 ± 5.9 ^C	2.4 ± 1.2 logs*
ARB^{CIP}	log (CFU/100 mL)	5.6 ± 0.5 ^A	2.9 ± 2.0 ^B	0.9 ± 1.8 ^B	2.7 ± 2.2 logs*
ARB^{AMX}	log (CFU/100 mL)	6.1 ± 0.4 ^A	4.3 ± 1.0 ^B	1.7 ± 2.5 ^B	2.4 ± 2.5 logs*
ARB^{CTX}	log (CFU/100 mL)	5.8 ± 0.6 ^A	4.2 ± 1.1 ^B	1.4 ± 2.2 ^B	2.0 ± 2.2 logs*

435 **Note:** I: influent; SE: secondary effluent; FE: final effluent; T: temperature; redox: oxidation-reduction potential; EC: electrical conductivity;
436 DO: dissolved oxygen; TU: turbidity; COD: chemical oxygen demand; NH₄⁺-N: ammonium nitrogen; NO₃⁻-N: nitrate as nitrogen; NO₂⁻-N:
437 nitrite as nitrogen; PO₄⁻³-P: phosphate as phosphorus, TC: total coliform; FC: fecal coliform; ARB^{CIP}: ciprofloxacin-resistant bacteria;
438 ARB^{AMX}: amoxicillin-resistant bacteria; ARB^{CTX}: ceftriaxone-resistant bacteria. (VF: n = 7, AS: n = 4, BD: n = 9, total = 20). Superscripts
439 "A", "B", and "C" denote statistically different distributions (Kruskal-Wallis/Dunnet tests). n/s, non-significant differences. *) The reductions of
440 microbiological and antibiotic resistance parameters were reported in log units. These values were calculated considering the average between
441 the different reductions obtained in the 20 WWTPs. **) For these parameters, removal efficiencies were calculated considering percentage
442 calculated by ((I-FE)/I) x 100%. These performances were calculated considering the average between the different removal efficiencies
443 obtained in the 20 WWTPs.

444 **Table 2.** Overall physicochemical and microbiological characterization of I, SE, and FE from the WWTPs monitored during Campaign 2.

445

Parameter	Unit	Overall			Final Reduction* or
		I	SE	FE	Removal Efficiencies**
					(%)
pH	-	7.0 ± 1.1	6.7 ± 0.4	6.6 ± 0.2	n/s
T	°C	14.0 ± 2.9	15.1 ± 2.8	15.1 ± 3.7	n/s
Redox	mV	54.1 ± 1.2	67.7 ± 172.6	157.7 ± 261.3	n/s
EC	µS/cm	1.2 ± 0.4	0.8 ± 0.4	0.9 ± 0.2	n/s
DO	mg/L	2.3 ± 1.8	3.3 ± 1.4	4.4 ± 1.8	n/s
TU	NTU	167.1 ± 48.2 ^A	26.3 ± 29.9 ^B	29.4 ± 21.4 ^B	82.5 ± 12.9 %**
COD	mg/L	314.0 ± 236.3 ^A	104.7 ± 96.0 ^B	52.1 ± 41.1 ^B	79.3 ± 20.7 %**
NH₄⁺-N	mg/L	58.9 ± 18.9 ^A	20.3 ± 11.1 ^B	12.3 ± 8.3 ^B	79.3 ± 12.4 %**
NO₃⁻-N	mg/L	2.3 ± 1.3	3.2 ± 3.5	3.6 ± 3.8	n/s
NO₂⁻-N	mg/L	0.2 ± 0.3	0.2 ± 0.1	0.3 ± 0.3	n/s
PO₄²⁻-P	mg/L	10.6 ± 8.4	5.9 ± 4.2	6.0 ± 2.7	n/s
TC	log (CFU/100 mL)	8.4 ± 0.7 ^A	6.1 ± 1.7 ^A	3.8 ± 1.7 ^C	4.5 ± 1.4 logs*

FC	log (CFU/100 mL)	7.3 ± 0.9 ^A	5.4 ± 1.2 ^A	3.2 ± 1.5 ^B	4.1 ± 1.4 logs*
ARB^{CIP}	log (CFU/100 mL)	5.6 ± 0.4 ^A	3.5 ± 1.4 ^B	2.7 ± 2.6 ^B	4.6 ± 1.1 logs*
ARB^{AMX}	log (CFU/100 mL)	6.1 ± 0.4 ^A	4.3 ± 0.9 ^B	5.0 ± 0.9 ^B	2.6 ± 0.4 logs*
ARB^{CTX}	log (CFU/100 mL)	5.8 ± 0.5 ^A	4.0 ± 1.1 ^B	3.5 ± 1.9 ^B	3.9 ± 0.4 logs*
16S	log (copies/100 mL)	8.3 ± 0.3 ^A	6.2 ± 1.2 ^B	5.2 ± 0.9 ^B	3.1 ± 0.8 logs*
<i>sulI</i>	log (copies/100 mL)	5.3 ± 0.3 ^A	4.3 ± 0.4 ^B	3.0 ± 1.2 ^B	2.3 ± 0.9 logs*
<i>intI1</i>	log (copies/100 mL)	5.6 ± 0.3 ^A	4.6 ± 0.8 ^A	2.7 ± 1.1 ^B	2.9 ± 1.0 logs*
<i>bla_{TEM}</i>	log (copies/100 mL)	3.6 ± 0.8 ^A	1.6 ± 0.5 ^B	1.1 ± 0.4 ^B	2.6 ± 0.5 logs*
<i>qnrS</i>	log (copies/100 mL)	3.7 ± 1.2 ^A	2.3 ± 1.5 ^B	1.9 ± 1.3 ^B	2.4 ± 0.5 logs*
<i>bla_{CTX-M-32}</i>	log (copies/100 mL)	3.1 ± 1.5 ^A	1.1 ± 0.5 ^B	< LOD ^C	3.4 ± 0.2 logs*
<i>tetM</i>	log (copies/100 mL)	5.0 ± 0.6 ^A	2.2 ± 0.5 ^B	< LOD ^C	4.0 ± 1.0 logs*

446 **Notes:** I: influent; SE: secondary effluent; FE: final effluent; T: temperature; redox: oxidation-reduction potential; EC: electrical conductivity; DO:
447 dissolved oxygen; TU: turbidity; COD: chemical oxygen demand; NH₄⁺-N: ammonium nitrogen; NO₃⁻-N: nitrate as nitrogen; NO₂⁻-N: nitrite as
448 nitrogen; PO₄³⁻-P: phosphate as phosphorus, TC: total coliform; FC: fecal coliform; ARB^{CIP}: ciprofloxacin-resistant bacteria; ARB^{AMX}: amoxicillin-
449 resistant bacteria; ARB^{CTX}: ceftriaxone-resistant bacteria, LOD: limit of detection, ^a: negative removal efficiencies (n = 6). Superscripts "A", "B", and
450 "C" denote statistically different distributions (Kruskal-Wallis/Dunnet tests). . *) The reductions of microbiological and antibiotic resistance parameters
451 were reported in log units. These values were calculated considering the average between the different reductions obtained in the 6 WWTPs. **) For
452 these parameters, removal efficiencies were calculated considering percentage calculated by ((I-FE)/I) x 100%. These performances were calculated
453 considering the average between the different removal efficiencies obtained in the 6 WWTPs.

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Figure Captions

455 **Figure 1.** Map of the sampled WWTPs, displaying their locations and corresponding biological
456 treatments. The following were sampled during Campaign 1: VF1: vermifilter in Copielemu, VF2:
457 vermifilter in Villa Cristo Redentor, VF3: vermifilter in Villa Las Almendras, VF4: vermifilter in
458 Villa Las Mercedes; VF5: vermifilter in Campamento; VF6: vermifilter in Llico; VF7: vermifilter in
459 Las Peñas; AS1: activated sludge in Rere, AS2: activated sludge in Río Claro, AS3: activated sludge
460 in Charrua, AS4: activated sludge in Tomeco; BD1: biodisc in Villa Laja; BD2: biodisc in Santa Fe;
461 BD3: biodisc in La Aguada; BD4: biodisc in Santa Rosa; BD5: biodisc in Pehuén; BD6: biodisc in
462 Antuco; BD7: biodisc in Canteras Sur; BD8: biodisc in Laraquete; BD9: biodisc in Coihue. The
463 resampled WWTPs during Campaign 2 – VF1, VF3, AS1, AS2, BD1, BD2 – are highlighted in red.

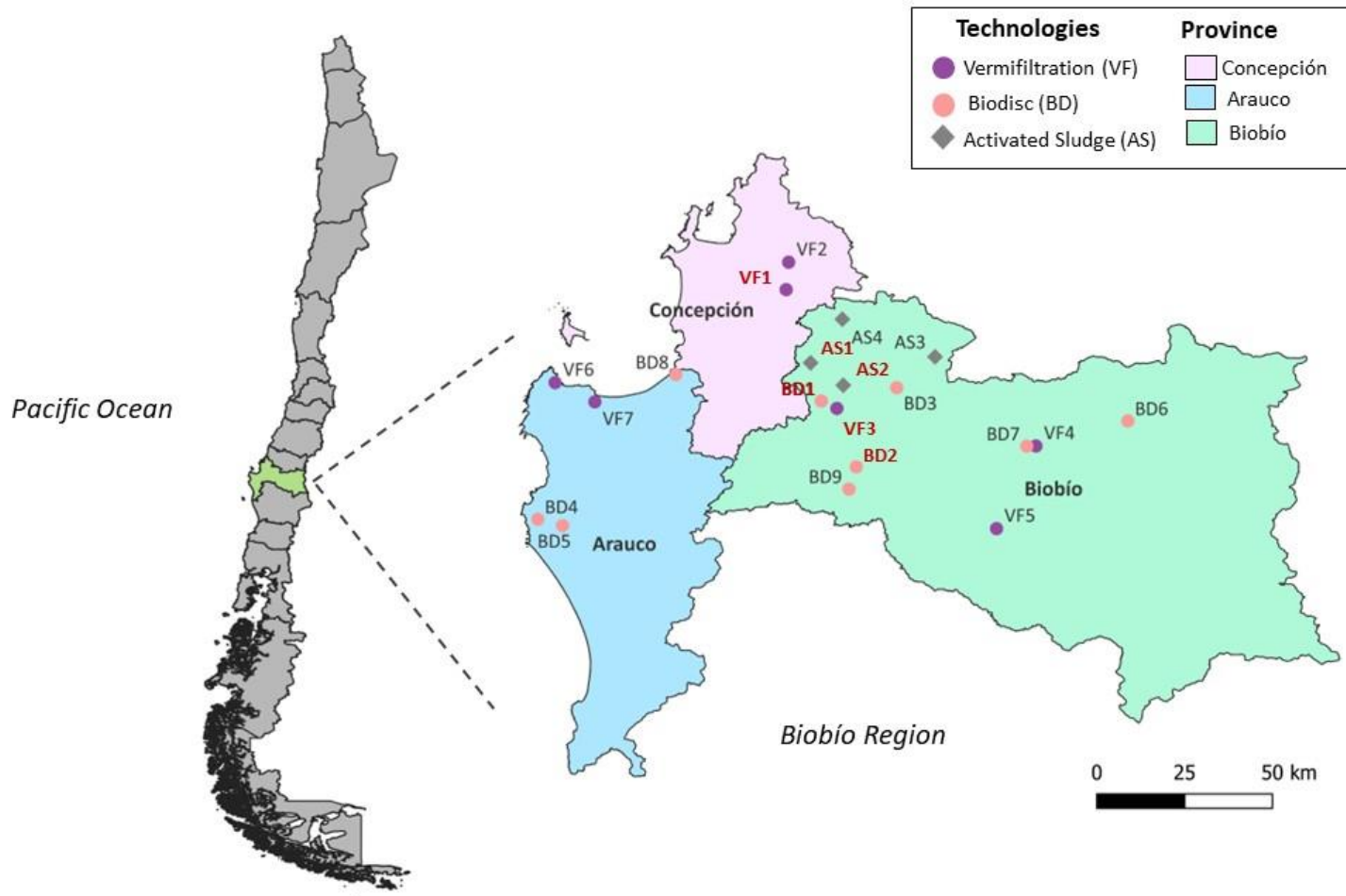
464 **Figure 2.** Schematic diagram of different biological and disinfection treatment technologies: a)
465 vermifiltration (VF); b) activated sludge (AS) and c) biodisc (BD).

466 **Figure 3.** Principal component analyses during Campaign 1: a) score plot and b) loading plot

467 **Figure 4.** Principal component analyses during Campaign 2: a) biplot; b) score plot and c) loading
468 plot

469 **Figure 5.** Reductions (relative to I) in microbiological parameters and ARGs in SE and FE from VF,
470 AS and BD during Campaign 2: a) TC, b) FC, c) *intI1*, d) *sul1*, and e) *tetM*. Boxes cover the interval
471 between the first and third quartiles of the distribution and the thick line indicates the median. See the
472 logarithmic scale on the Y-axis. Included *-values* relate to the comparison between SE and EF samples
473 (Kruskal-Wallis test).

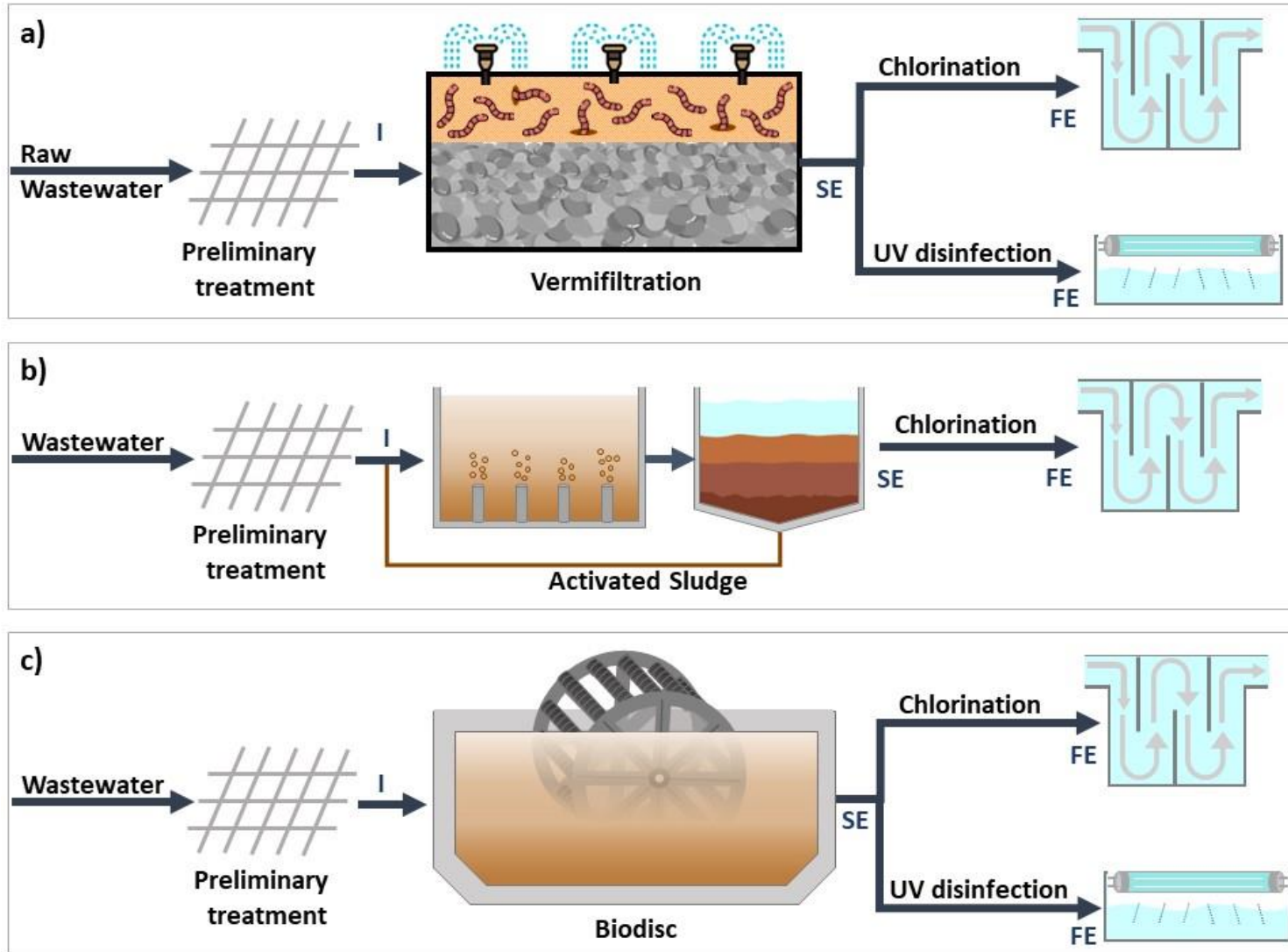
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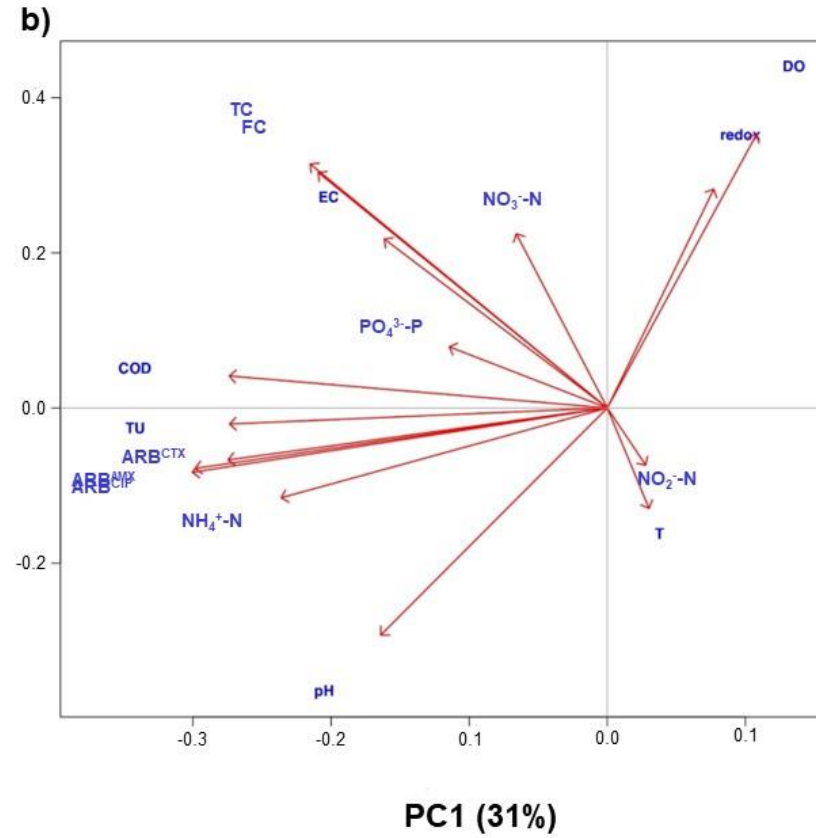
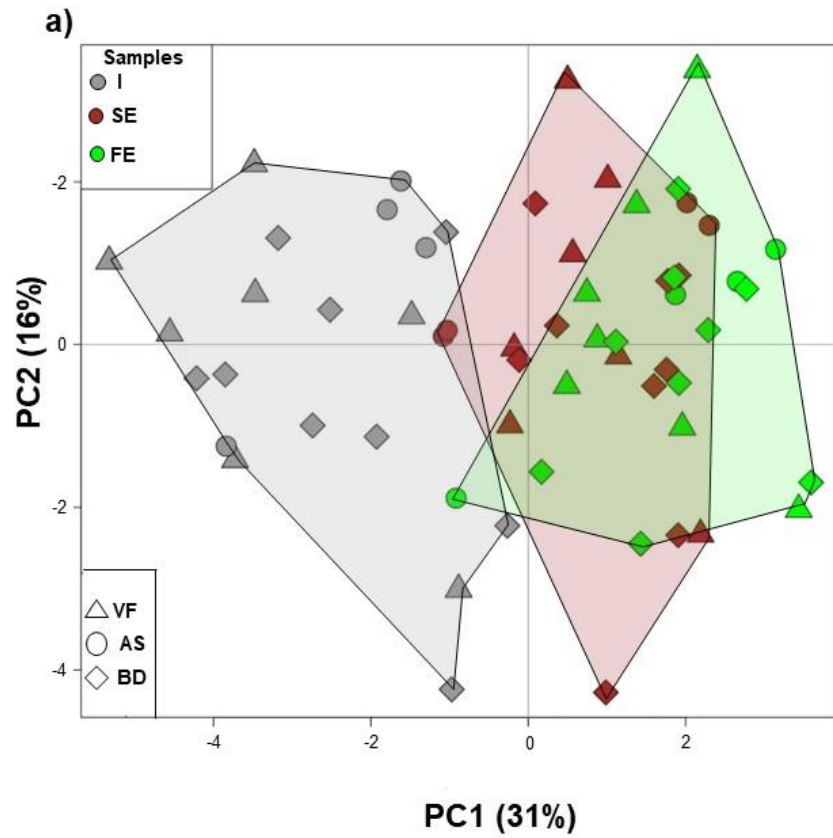
Figure 1



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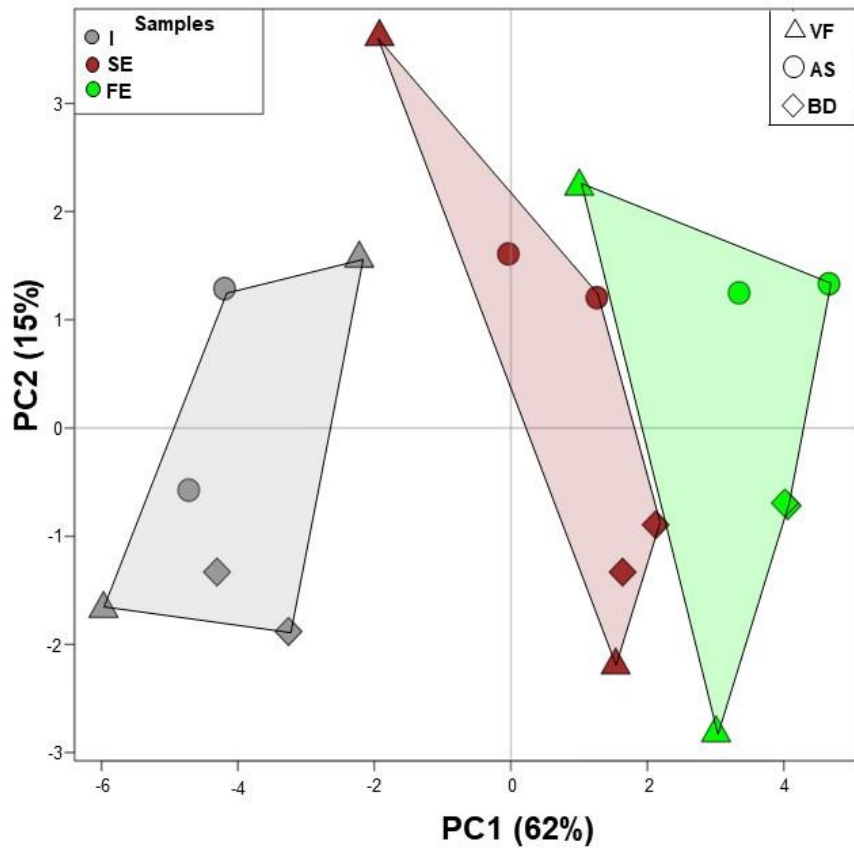
Figure 2



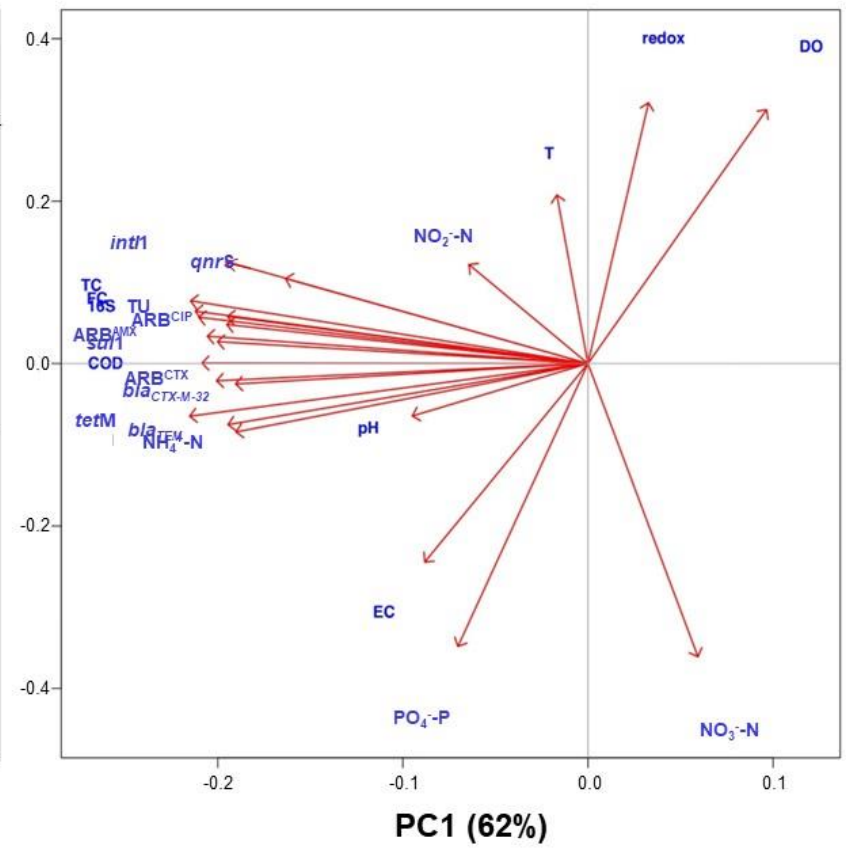
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Figure 3

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Figure 4

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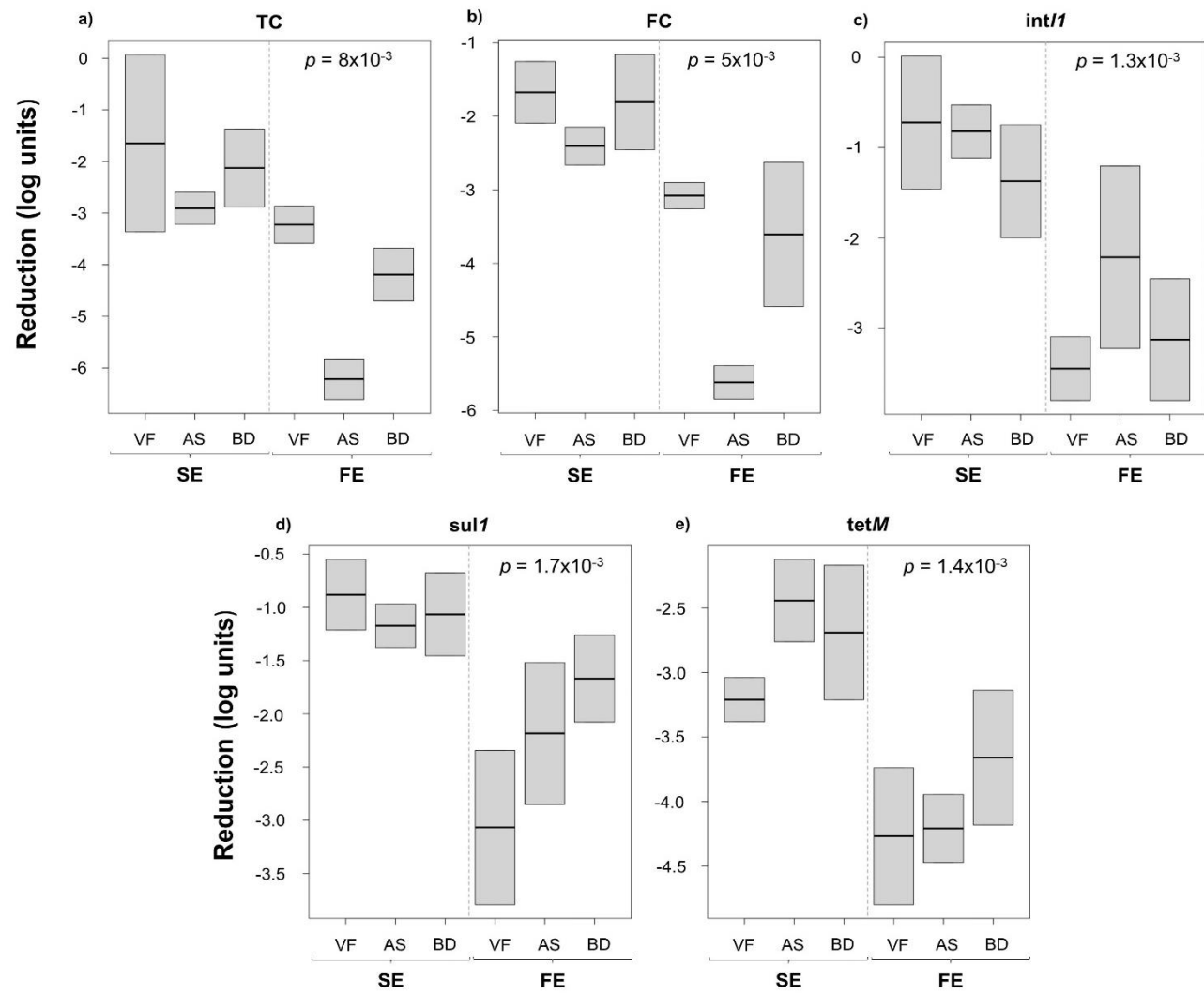


Figure 5