

**Heterotrophic activity in the active layer of a vermifilter used for sewage treatment:  
effects of worm density and seasonality**

Victor Gutiérrez<sup>1,2</sup>, Gloria Gómez<sup>1,2</sup>, Diana C. Rodríguez<sup>3</sup> and Gladys Vidal<sup>1,2\*</sup>

<sup>1</sup>Environmental Engineering & Biotechnology Group (GIBA-UDEC), School of Environmental  
Science, Universidad de Concepción, Concepción 4070386, Chile.

<sup>2</sup>Water Research Center for Agriculture and Mining, CRHIAM. ANID Fondap Center. Victoria  
1295, Concepción, Chile.

<sup>3</sup>Pollution Diagnostics and Control Group (GDCON), Environment School, Faculty of Engineering,  
University Research Campus (SIU), Universidad de Antioquia, Calle 70 No. 52-21, Medellin,  
Colombia.

Submitted to: *Journal of Environmental Chemical Engineering*

\*Corresponding author: Dr. Gladys Vidal

E-mail: glvidal@udec.cl

## Abstract

The active layer of a vermifilter (VF) is composed of woodchips that contain heterotrophic bacteria and worms capable of removing organic matter. However, there is no information on heterotrophic microbial kinetics related to oxygen uptake rate ( $OUR_{end}$ ), specific oxygen uptake rate ( $SOUR_{end}$ ), and heterotrophic biomass yield ( $Y_H$ ) as they relate to evaluating the removal of COD (chemical oxygen demand) and  $BOD_5$  (biochemical oxygen demand) from wastewater. The goal of this study was to assess the heterotrophic activity of the active layer of a full-scale VF that treats rural wastewater. In addition, the effects of seasonality and earthworm density were determined. Heterotrophic activity was evaluated with a respirometer using active layer (wood chip) samples with earthworm densities of  $1105 \pm 982$  earthworm/ $m^3$  (Zone A) and  $7221 \pm 1699$  earthworm/ $m^3$  (Zone B), in fall-winter and spring-summer. The results show that the VF has a  $Y_H$  of  $0.47 \pm 0.1$  and a growth rate ( $\mu_{max}$ ) of  $0.05 \pm 0.04 \text{ d}^{-1}$ . The  $Y_H$  value was 0.39 in fall-winter and 0.54 in spring-summer, while the  $\mu_{max}$  value was  $0.07 \text{ d}^{-1}$  in fall-winter and  $0.02 \text{ d}^{-1}$  in spring-summer.  $OUR_{end}$  and  $SOUR_{end}$  increased 95% more in spring-summer than in fall-winter and a 64% more in Zone B than Zone A. This increase in heterotrophic activity corresponds to increases of 15.6% in COD removal and 12.2% in  $BOD_5$  removal in spring-summer. These results indicate that seasonality and earthworm density affect kinetic parameters such as  $OUR_{end}$  and  $SOUR_{end}$ . Finally, the measurement of kinetic parameters allows the COD and  $BOD_5$  removal efficiency of a VF to be estimated.

**Keywords:** Sewage treatment; Active layer; Heterotrophic activity; Respirometry; Kinetic parameters

## 1. Introduction

According to the World Health Organization monitoring program, 6 out of every 10 people do not have access to safely managed sanitation services. This lack of coverage in final wastewater treatment generates water quality deterioration, loss of biodiversity, and unhealthy environments that lead to the transmission of diarrheal diseases such as cholera, dysentery, and typhoid fever [1,2]. Therefore, wastewater must be treated prior to its discharge, a process carried out by conventional wastewater treatment plants (WWTP), which use technologies that include activated sludge. However, this technology is unsuitable for rural areas with populations of density below 300 inhabitants per km<sup>2</sup>. In these areas, centralized technology has limitations such as the absence of sewerage system, energy costs for pumping systems, geographical and climatic limitations, low socioeconomic level, lack of technical assistance, skills to operate the systems. [3]. Therefore, it is necessary to find decentralized technologies that minimize the risks of wastewater discharges in these areas.

In such settings, vermifilters (VF) are an alternative to conventional WWTP. These nature-based systems operate with the synergistic activity of earthworms and microorganisms that change the physicochemical properties of wastewater [4]. The ingestion, burrowing, and excretion behaviors of earthworms reinforce this relationship, as they generate an aerated environment that promotes microorganism growth [5]. This facilitates the removal of organic matter, nutrients, and pathogens by aerobic microorganisms and reduces costs, as no injection pumps are used [6]. Some studies indicate that VF can reach removal efficiencies of 89.0% for organic matter measured as chemical oxygen demand (COD), 79.5% for total nitrogen, and 87.0% for total phosphorous [7, 8, 9]. However, as with any biological treatment systems, performance depends on operating conditions [10]. Earthworm density, temperature, filter

medium, hydraulic loading rate, and organic loading rate are design and operating parameters and thus key factors that affect the removal organic matter, removal nutrient and greenhouse gases that reach 1975.5 mg/m<sup>2</sup>h for CO<sub>2</sub>, 36.5 mg/m<sup>2</sup>h for CH<sub>4</sub> and 12.3 mg/m<sup>2</sup>h for N<sub>2</sub>O [5,7,11]. In a VF, biological processes occur in the active layer , a filter medium that facilitates the adsorption of nutrients from sewage (e.g phosphorus and nitrogen), and that contains autotrophic and heterotrophic microorganisms [12,13]. Some studies have indicated that over 90% of organic matter removal in an aerobic medium could be related to heterotrophic aerobic bacteria [12,14]. However, few studies have addressed the behavior and growth of the heterotrophic biomass of the active layer of a full-scale VF [15]. To assess how this design and operating parameters affect organic matter removal efficiency, respirometry techniques can be used to model, understand, and monitor the biological processes that occur in a VF based on the estimation of kinetic parameters of the heterotrophic aerobic biomass [16]. Respirometry is defined as the measurement of the biological consumption rate of an inorganic electron acceptor [17]. This technique allows the aerobic biological processes achieved by the microorganism biomass to oxidize an organic substrate to be reproduced at laboratory scale [10]. Therefore, the characterization of kinetic parameters of the aerobic biological process provides activity values for the heterotrophic biomass responsible for removing organic matter from wastewater in a WWTP [17,18]. The main kinetic parameters in this analysis are OUR<sub>end</sub>, SOUR<sub>end</sub>, Y<sub>H</sub>, and the maximum growth rate of the biomass ( $\mu_{\max}$ ). For example, in an activated sludge system, it has been observed that a high OUR<sub>end</sub> of 15.3 mgO<sub>2</sub>/L·h or low  $\mu_{\max}$  of 0.047 reflects problems in the system operating conditions or even indicates toxicity levels in the influent [19,20]. This type of analysis therefore provides information for modeling and optimizing the main aerobic processes that degrade organic matter via heterotrophic biomass growth [21]. The

respirometric method is one of the most widely used techniques for characterizing sewage and evaluating the microbial response in activated sludge systems [16]. However, it has proven to be highly effective in determining kinetic and stoichiometric parameters specific to particular types of biomasses, such as, moving bed biofilm reactor (MBBR) [17]. Therefore, although respirometry is a biological method used especially for activated sludge [18], technological advancements allow respirometry to be applied as a diagnostic tool in other types of unconventional plants [16], such as VF systems. Thus, the objective of this study is to use respirometry techniques to assess the heterotrophic activity of the active layer of a full-scale VF and determine the effects of seasonality and earthworm density on removal of the organic matter contained in wastewater.

## **2. Materials and Methods**

### **2.1 Design and operating conditions**

This study was carried out in a rural WWTP located in Copiulemu Commune, Concepción, in the Biobío Region, Chile. This region is a mediterranean climate. In dry months, rainfall reaches 35 mm and the temperature 25°C. In wettest month, rainfall reaches 350 mm and temperature from 0°C to 13°C [22,23]. This WWTP uses a sequential system that includes pretreatment for solids removal, followed by a VF and radiation ultraviolet for disinfection protected by a roof that covers the entire system. The VF is a vertical subsurface flow system, and its main characteristics are summarized in Table 1. Wastewater enters a rotary filter that has a helical screw to sweep solids from an external container to the VF. Once treated, this wastewater is stored in an accumulator tank and transferred via two pumps to the upper part of the VF, from where it is distributed over the surface via 24 sprinklers. The VF operates with a flow, hydraulic loading rate (HLR), and organic loading rate (OLR) of 160 m<sup>3</sup>/d, 0.6

m<sup>3</sup>/m<sup>2</sup>d, and 0.5 kgCOD/m<sup>2</sup>d, respectively. The filter material is stratified, with a lower layer of stones and an upper layer of wood chips measuring 0.92 ± 0.12 m. The latter layer is the active layer, where earthworms of the species *Eisenia foetida* and heterotrophic and autotrophic microorganisms are responsible for biological reactions [12,13]. The earthworm density was studied by taking samples between different seasons and different heights of the active layer. No differences were observed between seasons. Moreover, the Zone A of 104 cm and Zone B of 80 cm showed densities of 1105 ± 982 earthworm/m<sup>3</sup> and 7221 ± 1699 earthworm/m<sup>3</sup>, respectively.

### Table 1

## 2.2 Monitoring strategy

The monitoring strategy involved samples between May 2022 and November 2023, during the Southern Hemisphere fall-winter and spring-summer. Figure 1 shows a diagram with the VF and the active layer monitoring strategy. In Zones A and B of the VF, samples of the active layer were taken from different points by inserting a tube 12 cm in diameter and 100 cm in length. Wood chips were collected from the inside of the tube to calculate the earthworm density. Wastewater samples were taken from the pretreatment outlet (IN), the VF outlet (E1), and the UV outlet (E2). All samples were kept at a temperature of 4°C for less than 24 h until their analysis [24,25].

### Figure 1

### 2.3 Analysis of liquid samples

The liquid samples – IN, E1, and E2 – were filtered with a Whatman membrane with a pore size of 0.7  $\mu\text{m}$  and analyzed according to the protocol described in the standard method [26]. The organic matter present in the samples was determined by measuring COD (colorimetric method, 5220-D) and biological oxygen demand ( $\text{BOD}_5$ ) (azide-modified Winkler method, 5210-B).

### 2.4 Respirometry analysis

The respirometry experiments were carried out to determine the kinetic response of the heterotrophic microorganisms in the active layer [16]. The respirometry test was applied to the solid samples of Zone A ( $1105 \pm 982 \text{ worm/m}^3$ ) and Zone B ( $7221 \pm 1699 \text{ worm/m}^3$ ) of the VF.

### *Figure 1*

Wood chip biofilm was used to analyze the active layer. The solid sample was diluted in distilled water at a proportion of 1:20 to obtain concentrations in ranges of 1000-2000  $\text{mgSSV/L}$  [10,25]. The experiment was performed using a BM-T respirometer. This is a batch method that includes a recirculation pump, with two experiments carried out: static  $\text{OUR}_{\text{end}}$  and  $\text{SOUR}_{\text{end}}$  mode, which determines the endogenic oxygen uptake rate of the biomass, and dynamic R mode, which analyzes the evolution of the oxygen uptake rate to degrade an exogenous biodegradable substrate (sodium acetate). The samples were placed in a 1-liter tank in endogenous conditions to begin the experiment at a constant temperature of  $20 \pm 1^\circ\text{C}$ . The device allows agitation and aeration and includes an oximeter that measures

and records data in BM-Advance software [10]. To assess the kinetic parameters of the heterotrophic activity, the autotrophic species were inhibited with 1-4 mg/ml of allylthiourea (ATU). Table 2 shows the main kinetic parameters related to heterotrophic activity that were calculated via BM-Advance, which is integrated into the device.

**Table 2**

## **2.5 Statistical analysis**

To assess the effects of seasonality on COD, BOD<sub>5</sub>, and the kinetic parameters OUR<sub>end</sub> and SOUR<sub>end</sub>, statistical analyses were performed using RStudio version 4.3.2, with a significance level of  $p = 0.05$ . Shapiro–Wilk and Levene tests were carried out to analyze the normality and homogeneity of variance, respectively. Subsequently, an ANOVA test was performed [27].

## **3. Results and discussion**

### **3.1 Kinetic parameters and heterotrophic activity of the active layer**

Table 3 shows the main kinetic parameters of heterotrophic biomasses from different wastewater treatment plants: OUR<sub>end</sub> (mgO<sub>2</sub>/L·h), SOUR<sub>end</sub> (mgO<sub>2</sub>/gVSS·h), Y<sub>H</sub> (mgCOD<sub>m</sub>/COD<sub>s</sub>);  $\mu_H$  (d<sup>-1</sup>),  $\mu_{max}$  (d<sup>-1</sup>), and K<sub>d</sub> (d<sup>-1</sup>). The kinetic parameters in the VF presented variations with respect to other types of technology.

**Table 3**

### 3.1.1 Oxygen consumption ( $OUR_{end}$ and $SOUR_{end}$ )

In the VF  $OUR_{end}$  was  $1.22 \pm 0.59$   $mgO_2/L \cdot h$  and  $SOUR_{end}$  was  $1.24 \pm 0.63$   $mgO_2/gVSSh$ . These values are within the ranges observed in plants used for wastewater treatment such as CAS, UCT-MBR, and UASB-MBR which presented  $OUR$  values between 1.6 and 6  $mgO_2/L \cdot h$ . [10, 20, 28]. In the CAS studied by Arias et al. [19],  $OUR_{end}$  reached 15.3  $mgO_2/L \cdot h$ . This increase is caused by an overload of the heterotrophic biomass that affects wastewater treatment efficiency [19]. In the case of the CAS studied by Abdi et al. [15],  $OUR_{end}$  reached 0.05  $mgO_2/L \cdot h$ . Low values are explained by toxic substances present in the influent (i.e., sulfides) that affect biomass activity. Variations in  $OUR_{end}$  and  $SOUR_{end}$  allow the metabolic function of heterotrophic microorganisms to be evaluated [20] and associated with different operating conditions to quantify and detect possible disturbances in a VF (i.e., influent retention times and organic loading rate, [19, 30]. Regarding organic loading rate (OLR), Llamas et al. [10] determined in a UASB-MBR that an OLR of 0.4  $KgCOD/m^3d$  generates maximum  $OUR$  values ranging from 1.65  $mgO_2/L \cdot h$  to 2.61  $mgO_2/L \cdot h$ . At 0.7  $KgCOD/m^3d$ , the  $OUR$  decreases due to system stabilization problems and at 0.2  $KgCOD/m^3d$  the  $OUR$  decreases due to lack of substrate for microorganism growth [31,32]. In the case of the studied VF, the OLR was 0.54  $KgCOD/m^3d$ ; this design parameter is within the optimum range for this type of technology (0.2-0.6  $KgCOD/m^3d$ ) [5]. When the OLR is below 0.2  $kgCOD/m^3d$ , the growth of autotrophs outcompetes the growth of heterotrophs due to the limitation of organic carbon. This could reduce the COD removal efficiency below 77% [5]. Therefore, in VF the  $OUR_{end}$  and  $SOUR_{end}$  can be used to determine the optimal design and operating parameters that affect the active layer [7,33,34] and organic matter degradation processes [5,35].

### 3.1.2 Yield coefficient ( $Y_H$ )

The  $Y_H$  in the VF was  $0.47 \pm 0.11$  mgCODm/CODs. This parameter is below the 0.6-0.8 mgCODm/CODs range of CAS, OSA, UCT-MBR, and UASB-MBR [20]. Abdi et al. [15], in a CAS, found low  $Y_H$  values, which reached 0.2 mgCODm/CODs due to the toxic effect of sulfides. Therefore, if the influent has no toxic effect,  $Y_H$  indicates the capacity of the system to generate biomass via heterotrophic activity [15]. In a VF, this process occurs in the active layer, which contains earthworms and microorganisms that form the biofilm [13]. Di Trapani et al. [29] compared the heterotrophic and autotrophic activity of the biofilm and suspended biomass in an IFAS-MBR. This study found that systems with suspended biomass promote heterotrophic activity, with a  $Y_H$  of 0.66, whereas systems with biofilm promote autotrophic activity, with a  $Y_A$  of 0.47. These differences can be explained by the trade-off that exists between microorganisms. For example, in MBBR stabilized promotes autotrophs of slow-growing specialized in nitrification achieving  $Y_A$  of 0.6 and  $Y_H$  of 0.45 [36]. Otherwise, in MBR (Membrane bioreactors), promotes heterotrophs of fast-growing specialized in removing organic matter achieving  $Y_H$  of 0.46 and  $Y_A$  of 0.18 [23,28,29].

### 3.1.3 Growth rate ( $\mu_H$ ) and endogenous decay constant ( $K_d$ )

The  $\mu_{\max}$  in the VF was  $0.05 \pm 0.04$  d<sup>-1</sup>. This parameter is below the 0.4 – 9 d<sup>-1</sup> range of CAS, OSA, UCT-MBR and UASB-MBR [10,20,29]. In CAS, Dehnavi et al. [20] and Abdi et al. [15] also found low values between 0.047-0.17 d<sup>-1</sup>. This value is related to system operating conditions (i.e., influent toxicity, sludge state, hydraulic retention times). Regarding the VF, low  $\mu_{\max}$  values are explained by the low growth of the heterotrophic biomass due to the type of microbiome that develops in the active layer. Earthworms in a VF promote the development of heterotrophic microorganisms that participate in the degradation of organic

matter and autotrophic microorganisms that participate in nitrification processes [11,37, 38]. The two microorganism types compete in the active layer and respond to different growth kinetics [39]. Leyva et al. [21] found that the immobilized biomass of the biofilm presents an autotrophic  $\mu_{\max}$  of 0.6-0.7 d<sup>-1</sup> and heterotrophic  $\mu_{\max}$  of 0.02-0.11 d<sup>-1</sup>, near the heterotrophic  $\mu_{\max}$  of the VF. Whereas heterotrophs grow quickly and depend on organic carbon sources, autotrophs grow slowly and depend on inorganic carbon sources [40,41]. Meanwhile, the earthworm gut acts as a reserve of denitrifying microorganisms. In the presence of nitrates, nitrites, and organic carbon of the medium, different facultative anaerobic denitrifiers survive in the external environment and compete with the microbiological community [5,7]. Oxygen is another factor that limit  $\mu_{\max}$  in a VF, the burrowing behavior of earthworms introduces between 0.6 and 0.9 mg/L of oxygen in the active layer [42]. In contrast, moving bed biofilm reactors (MBBRs) can achieve oxygen concentrations between 1.5 and 5 mg/L through mechanical aeration, which enhances cellular synthesis within the biofilm [43]. With respect to kinetic parameter  $K_d$ , it is related to biomass loss and microorganism decay rate. The VF presented a loss of 3±1% of the biomass that developed in the active layer, which is among the characteristics of the microorganism and earthworm consortium [10]. In a VF there are various processes such as endogenous decay of microorganisms, destruction of extracellular polymeric substances, selection of slow-growing bacteria, and predation of bacteria by higher organisms such as earthworms [16,44,45]. This biomass loss is counteracted by humic substances and the retention capacity of the active layer [33,46], which promotes the development of the microbial community [47,48], generating an equilibrium between biomass growth and the loss rate.

### 3.2 Effects of seasonality on heterotrophic activity

Table 4 shows the kinetic parameters of the heterotrophic biomass in different seasons. The  $OUR_{end}$  (mg/L·h) and  $SOUR_{end}$  (mg/gVSSh) parameters increased more than 95% in spring-summer relative to fall-winter. In a VF the main mechanisms that determine the removal of organic matter are related to the activity of earthworms that accelerate the development of the microbial community [5]. *Eisenia fétida* is a poikilothermic species that lives in an optimum range of 15-20°C [49]. Therefore, temperatures within this range improve the symbiotic relationship between the earthworms and heterotrophic microorganisms that determine organic matter removal [50]. This explains the increase in  $Y_H$  from 0.39 to 0.54 mgCODm/mgCODs. This increase in the heterotrophic biomass is consistent with other studies in which increases in COD removal of 6% to 15% in warm periods were observed [11,50]. However, in the early years of the VF, physical processes such as the adsorption mechanisms of the woodchip could maintain COD removal efficiency between 65% and 88% without season difference [8,31]. Meanwhile, kinetic parameter  $\mu_{max}$ , decreased from 0.07 d<sup>-1</sup> in fall-winter to 0.02 d<sup>-1</sup> in spring-summer and  $K_d$  increased from 0.02 d<sup>-1</sup> in fall-winter to 0.04 d<sup>-1</sup> in spring-summer. These differences in  $K_d$  could be due to toxic compounds such as antibiotics in wastewater [11,51]. For example, Bermúdez et al. [52] and Dehnavi et al. [20] have found that there is a decrease in  $\mu_{max}$  and variations in  $K_d$  in the presence of antibiotics. This compound toxic can increase the energy required for generating specific inactivating enzymes to prevent the toxic effects, this could decrease  $\mu_{max}$  from 0.04 to 0.005 [20,30], while maintaining OUR of 2.25 mg/Lh and  $Y_H$  of 0.54. Besides, variations observed in these kinetic parameters can also be produced by operating conditions in the VF [28]. En spring-summer, a decrease of 90% in rainfall [22], combined with population fluctuation in tourist

areas [53], can raise the organic loading rate (OLR), from 0.2 to 5.1 kg COD/m<sup>2</sup>·d [54]. The elevated OLR, driven by the increased influx of organic matter, clog the pores of the vermifilter and reduce the oxygen available in the system [55]. In extreme dissolved oxygen deficit, the aerobic bacterial population might undergo an endogenous phase [56] and restrict the growth of microorganisms,  $\mu_{\max}$ .

#### **Table 4**

### **3.3 Effects of earthworm density on heterotrophic activity**

Figure 2 shows significant differences between the seasons and monitored zones for OUR<sub>end</sub> and SOUR<sub>end</sub>. In winter and spring, Zone B (7221 ± 1699 earthworm/m<sup>3</sup>) presented greater oxygen uptake rates than Zone A (1105 ± 982 earthworm/m<sup>3</sup>), with an increase in OUR of over 80% and an increase in SOUR of over 64%. Earthworm density is a VF design parameter [11, 57]. Earthworms can directly affect the formation of the biofilm, determining its morphology and final composition [7,33]. The body of the earthworm excretes stable aggregates and a mucus that increases the bacterial biodiversity involved in the degradation of organic matter from 0.8 to 1.1, according to the Shannon index [58]. Furthermore Li et al., 2013 [44], found that VF increases enzymatic activity between 9%-214% for protease, 11%-22% for dehydrogenase, 18%-32% for lipase, 12%-35% for amylase [59,60]. Therefore, a medium with greater earthworm density promotes the development of the active layer biofilm and can modify kinetic parameters [10,61]. Zones with a greater earthworm quantity generate environments with dissolved and colloidal organic matter that allow microorganisms to survive, reproduce, and form the biofilm [11,44,61].

### Figure 3

#### 3.4. Organic matter removal and heterotrophic activity in the VF

Figure 3 shows the COD and BOD<sub>5</sub> concentrations in IN, E1, and E2 of the VF in fall-winter and spring-summer, along with the oxygen uptake rate (OUR<sub>end</sub>). The COD removal efficiency in the VF was 64.4% - 80.9% and the BOD<sub>5</sub> removal efficiency was 77.6% - 91.5%. A comparison of efficiency levels between seasons reveals no significant differences in E1: 284±77 mg/L (64.4%) for COD and 134±38 mg/L (77.6%) for BOD<sub>5</sub> in fall-winter and 332±55 mg/L (64.0%) for COD and 115±41 (82.6%) mg/L for BOD<sub>5</sub> in spring-summer. This is related to the decrease in the adsorption capacity of the active layer due to excessive VF operating times without cleaning or change of the filter medium [62]. In this case, solids increase in E1 settle quickly in the outlet chamber, which can occur when cleanings are more than eight months apart [63]. By contrast, significant differences were found in effluent E2: 266±47 mg/L (65.3%) for COD and 132±45 mg/L (79.3 %) for BOD<sub>5</sub> in fall-winter and 173±29 mg/L (80.9%) for COD and 55±27 mg/L for BOD<sub>5</sub> (91.5%) in spring-summer. As mentioned, *Eisenia fetida* lives in an optimal range of 15-20°C [49]; therefore, temperatures outside this range affect the synergy between the earthworm and the aerobic microorganism consortium responsible for organic matter degradation [50]. In this study, the temperature was 11±2°C in fall-winter and 17±4°C in spring-summer. This difference affects the metabolic activity of the earthworms and the symbiotic relationship with microorganisms that facilitate organic matter removal. However, the adaptability of earthworms to survive within a temperature range of 5–29°C and a pH range of 4.5–9 helps maintain system robustness, achieving removal efficiencies of 65.3–80.9% for COD and 79.3–91.5% for

BOD<sub>5</sub>. [11]. The foregoing is consistent with the increase in OUR<sub>end</sub> in the active layer, which went from 1.0 mgO<sub>2</sub>/gL·h in fall-winter to 1.6 mgO<sub>2</sub>/gL·h in spring-summer. Therefore, the increase in heterotrophic activity can facilitate COD and BOD<sub>5</sub> removal in the VF in spring-summer [5]. It can thus be concluded that the measurement of OUR allows the organic removal capacity of a VF to be estimated.

### 3.5 Sustainable design

The economic sustainability of the vermifiltration technology has also been enlightened by creating a bridge with the concept of circular bio-economy [39]. However, the lack of standardized systems significantly reduces the likelihood of valorizing solid waste or sewage without compromising public health. With a HLR of 0.6 m<sup>3</sup>/m<sup>2</sup>·d and an OLR of 0.54 kg COD/m<sup>3</sup>·d, the VF achieved a removal efficiency of 173 mg/L (65.3%) and 266 mg/L (80.9%) for COD. These values are below those reported in other studies, which have shown removal efficiencies ranging from 77.3% to 89.0% with HLR below 2 m<sup>3</sup>/m<sup>2</sup>·d and OLR between 0.2–0.6 kg COD/m<sup>3</sup>·d [5]. On the other hand, Gutiérrez et al. [11] observed that VF systems do not remove Fecal Coliforms (FC) to safe levels in the effluents (i.e. 6.9 log<sub>10</sub> MPN/100 mL). Therefore, the concentrations of COD and FC discard sewage reuse as a viable option for irrigation [64]. Regarding the active layer, although some authors suggest that the vermicompost generated by earthworms can be applied to agricultural soils to utilize adsorbed nutrients such as nitrogen and phosphorus [4,39], there is still insufficient evidence to demonstrate effective pathogen reduction in these solids without additional treatment [5]. Concerning emissions, few studies have assessed the impact of these systems on Greenhouse Gas generation [3]. Specifically in VF systems, Zhao et al. [7] and Huang et al. [65] demonstrated that these systems can generate emissions of up to 1975.5 mg/m<sup>2</sup>·h of CO<sub>2</sub>,

36.5 mg/m<sup>2</sup>·h of CH<sub>4</sub>, and 12.3 mg/m<sup>2</sup>·h of N<sub>2</sub>O. In these systems, CO<sub>2</sub> is produced through organic matter oxidation under aerobic conditions; CH<sub>4</sub> through organic matter reduction in anaerobic conditions [55] and N<sub>2</sub>O is generated via nitrification and denitrification of nitrogen compounds present in sewage [66].

#### 4. Conclusions

Considering the results of this study, the following can be concluded:

- The microorganism growth rate in the system has a  $Y_H$  value of 0.39-0.54 mgCODm/CODs and a  $\mu_{max}$  of 0.02-0.07 d<sup>-1</sup>.
- Earthworm density affects kinetic parameters  $OUR_{end}$  and  $SOUR_{end}$ . Zone B ( $7221 \pm 1699$  earthworm/m<sup>3</sup>) promotes heterotrophic species activity and generates increases of over 64% in  $OUR_{end}$  and  $SOUR_{end}$  with respect to Zone A ( $1105 \pm 982$  earthworm/m<sup>3</sup>).
- Seasonality affects heterotrophic species activity. Under temperature values of  $17 \pm 4^\circ\text{C}$  in spring-summer, the kinetic parameters  $OUR_{end}$  and  $SOUR_{end}$  increased by 95% in the VF compared to fall-winter. Furthermore, the COD removal efficiency increased by 15.6% and BOD<sub>5</sub> removal efficiency increased by 12.2% in spring-summer.

## **Acknowledgments**

This work was supported by ANID/FONDAP/1523A0001. V. Gutiérrez thanks ANID/Scholarship Program/DOCTORADO NACIONAL/2021-21211494 for his scholarship.

## ***Author contributions***

**Gutiérrez, V.:** Compilation and analysis of information, original draft, methodology, writing, review, and editing. **Gomez, G.:** Layout and graphic design and image editing. **Rodríguez D.C.:** Review and editing. **Vidal, G.:** Conceptualization, validation, research, resources, original draft, writing, review and editing, visualization, supervision, and project administration.

## ***Declaration of competing interest***

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

## References

- [1] A.M. Leiva, G. Gómez, G. González-Rocha, B. Piña, G. Vidal, Performance of full-scale rural wastewater treatment plants in the reduction of antibiotic-resistant bacteria and antibiotic resistance genes from small-city effluents. *J. Environ. Chem. Eng.* 12 (2) (2024) 112322. <https://doi.org/10.1016/j.jece.2024.112322>.
- [2] World Health Organization (WHO), Technical Brief on Water, Sanitation, Hygiene and Wastewater Management to Prevent Infections and reduce the Spread off Antimicrobial Resistance, Switzerland, 2020.
- [3] N. Lourenço, L.M. Nunes, Review of dry and wet decentralized sanitation technologies for rural areas: applicability, challenges and opportunities, *Environ. Manag.* 65 (5) (2020) 642-664. <https://doi.org/10.1007/s00267-020-01268-7>.
- [4] S. Arora, S. Saraswat, Vermifiltration as a natural, sustainable, and green technology for environmental remediation: A new paradigm for wastewater treatment process, *Curr. Res. Green Sustain. Chem.* 4 (2021) 1-6. <https://doi.org/10.1016/j.crgsc.2021.100061>.
- [5] V. Gutiérrez, G. Gómez, D. Rodríguez, G. Vidal, Critical analysis of wastewater treatment using vermifilters: Operating parameters, wastewater quality, and greenhouse gas emissions. *J. Environ. Chem. Eng.* 11 (2023) 109683. <https://doi.org/10.1016/j.jece.2023.109683>.
- [6] L. Jiang, Y. Liu, X. Hu, G. Zeng, H. Wang, L. Zhou, X. Tan, B. Huang, S. Liu, The use of microbial-earthworm ecofilters for wastewater treatment with special attention to influencing factors in performance: A review, *Bioresour. Technol.* 200 (2016) 999-1007. <https://doi.org/10.1016/j.biortech.2015.11.011>.
- [7] Y. Zhao, Y. Zhang, Z. Ge, C. Hu, H. Zhang, Effects of influent C/N ratios on wastewater nutrient removal and simultaneous greenhouse gas emission from the combinations of vertical subsurface flow constructed wetlands and earthworm eco-filters for treating synthetic wastewater, *Environ. Sci. Process. Impacts.* 16 (3) (2014) 567-575. <https://doi.org/10.1039/c3em00655g>.
- [8] N. Pous, A. Barcelona, L. Sbardella, O. Gili, M. Hidalgo, J. Colomer, T. Serra, V. Salvadó, Vermifilter and zooplankton-based reactor integration as a nature-based system for

wastewater treatment and reuse. *Case Stud. Chem. Environ. Eng.* 4 (2021) 100153.  
<https://doi.org/10.1016/j.cscee.2021.100153>.

[9] J. Wang, X. Tang, Y. Liu, B. Xie, G. Li, H. Liang, Self-sustained ultrafiltration coupling  
 vermifiltration for decentralized domestic wastewater treatment: Microbial community and  
 mechanism. *Resour. Conserv. Recy.* 177 (2022)  
<https://doi.org/10.1016/j.resconrec.2021.106008>.

[10] M.J. Moya-Llamas, M.G. Pacazocchi, A. Trapote, Respirometric tests in a combined  
 UASB-MBR system treating wastewater containing emerging contaminants at different  
 OLRs and temperatures: Biokinetic analysis. *J. Environ. Manage.* 345 (2023) 118643.  
<https://doi.org/10.1016/j.jenvman.2023.118643>.

[11] V. Gutiérrez, N. Monsalves, G. Gómez, G. Vidal, Performance of a full-scale vermifilter  
 for sewage treatment in removing organic matter, nutrients, and antibiotic-resistant bacteria,  
*Sustainability.* 15 (2023) 6842. <https://doi.org/10.3390/su1508684>.

[12] C. Chicaiza, L. Huaraca, C.E. Almeida-Naranjo, V.H. Guerrero, C.A. Villamar,  
 Improvement of organic matter and nutrient removal from domestic wastewater by using  
 intermittent hydraulic rates on earthworm–microorganism biofilters, *Water Sci. Technol.* 82  
 (2) (2020) 281-291. <https://doi.org/10.2166/wst.2020.139>.

[13] A. Tahar, J. Feighan, L. Hannon, E. Clifford, Optimization of operational conditions and  
 performances of pilot scale lumbrifiltration for real raw municipal wastewater treatment,  
*Environ. Sci. Pollut. Res.* 29 (22) (2022) 32717-32731. <https://doi.org/10.1007/s11356-021-18259-8>.

[14] L. Wang, Z. Zheng, X. Luo, J. Zhang, Performance and mechanisms of a microbial  
 earthworm ecofilter for removing organic matter and nitrogen from synthetic domestic  
 wastewater, *J. Hazard. Mater.* 195 (2011) 245-253.  
<https://doi.org/10.1016/j.jhazmat.2011.08.035>.

[15] J. Abdi, S.H. Esmaeili-Faraj, M.N. Esfahany, Evaluation of the performance of an  
 activated sludge bioreactor for the sulfide removal in the presence of nanoparticles: Kinetic  
 study and respirometry test, *J. Nanostruct.* 13(1) (2023) 37-47.  
<https://doi.org/10.22052/jns.2023.01.005>.

- [16] A. Karlikanovaite-Balikci, N. Yagci, Determination and evaluation of kinetic parameters of activated sludge biomass from a sludge reduction system treating real sewage by respirometry testing, *J. Environ. Manage.* 240 (2019) 303-310. <https://doi.org/10.1016/j.jenvman.2019.03.131>.
- [17] M. Mainardis, M. Buttazzoni, M. Cottes, A. Moretti, D. Goi, 2021. Respirometry tests in wastewater treatment: Why and how? A critical review. *Sci. Total. Environ.* 793, 148607. <https://doi.org/10.1016/j.scitotenv.2021.148607>.
- [18] J. Zhang, Y. Shao, G. Liu, L. Qi, H. Wang, X. Xu, S. Liu, Wastewater COD characterization: RBCOD and SBCOD characterization analysis methods. *Sci. Rep.* 11 (2021) 691. <https://doi.org/10.1038/s41598-020-80700-8>.
- [19] M. Arias-Navarro, M. Villen-Guzman, R. Perez-Recuerda, J.M. Rodriguez-Maroto, The use of respirometry as a tool for the diagnosis of waste water treatment plants. A real case study in Southern Spain. *J. Water. Process. Eng.* 29 (2019) 100791. <https://doi.org/10.1016/j.jwpe.2019.100791>.
- [20] A.H. Dehnavi, M.M. Amin, A. Fatehizadeh, H.M. Attar, K. Ebrahimpour, B. Bina, Assessment of toxicity and kinetic effects of erythromycin on activated sludge consortium by fast respirometry method, *Environ. Health Eng. Manag.* 8 (3) (2021) 205-214. <https://doi.org/10.34172/ehem.2021.24>.
- [21] J.C. Leyva-Díaz, K. Calderón, F.A. Rodríguez, J. González-López, E. Hontoria, J.M. Poyatos, Comparative kinetic study between moving bed biofilm reactor-membrane bioreactor and membrane bioreactor systems and their influence on organic matter and nutrients removal, *Biochem. Eng. J.* 77 (2013) 28-40. <https://doi.org/10.1016/j.bej.2013.04.023>.
- [22] I. Vera, K. Saez, G. Vidal, Performance of 14 full-scale sewage treatment plants: comparison between four aerobic technologies regarding effluent quality, sludge production and energy consumption. *Environ. Technol.* 34 (2013), 2267-2275. <http://doi.org/10.1080/09593330.2013.765921>.
- [23] M.A. Doussoulin-Guzmán, F.J. Pérez-Porras, P. Triviño-Tarradas, A.F. Ríos-Mesa, A. García-Ferrer Porras, F.J. Mesas-Carrascosa, Grassland Phenology Response to Climate

518 Conditions in Biobio, Chile from 2001 to 2020, *J. Remote. Sens.* 14 (2022), 475.  
519 <https://doi.org/10.3390/rs14030475>.

520 [24] D. Lopez, M. Sepulveda-Mardones, N. Ruiz-Tagle, K. Sossa, E. Uggetti, G. Vidal.  
521 Potential methane production and molecular characterization of bacterial and archaeal  
522 communities in a horizontal subsurface flow constructed wetland under cold and warm  
523 seasons, *Sci. Total. Environ.* 648 (2019) 1042-1051.  
524 <https://doi.org/10.1016/j.scitotenv.2018.08.186>.

525 [25] A. Evangelou, D. Komilis, A new liquid-phase method and its comparison to two solid-  
526 phase microbial respiration activity methods to assess organic waste stability, *Waste Manag.*  
527 102 (2020) 1-11. <https://doi.org/10.1016/j.wasman.2019.10.011>.

528 [26] Standard methods for the Examination of Water and Wastewater (APHA). American  
529 Public Health Association. Washington, DC, USA, 2022.

530 [27] V. Carrillo, C. Collins, J. Brisson, G. Vidal, Evaluation of long-term phosphorus uptake  
531 by *Schoenoplectus californicus* and *Phragmites australis* plants in pilot-scale constructed  
532 wetlands. *Int. J. Phytoremediation*, 24(6) (2021) 610–621.  
533 <https://doi.org/10.1080/15226514.2021.1960478>.

534 [28] D. Di Trapani, M. Capodici, A. Cosenza, G. Di Bella, G. Mannina, M. Torregrossa, G.  
535 Viviani, Evaluation of biomass activity and wastewater characterization in a UCT-MBR pilot  
536 plant by means of respirometric techniques, *Desalination*. 269 (2011) 190-197.  
537 <https://doi.org/10.1016/j.desal.2010.10.061>.

538 [29] D. Di Trapani, G. Mannina, G. Viviani, Membrane Bioreactors for wastewater reuse:  
539 Respirometric assessment of biomass activity during a two year survey, *J. Clean. Prod.* 202  
540 (2018) 311-320. <https://doi.org/10.1016/j.jclepro.2018.08.014>.

541 [30] J.H. Guo, Y.Z. Peng, C.Y. Peng, S.Y. Wang, Y. Chen, H.J. Huang, Z.R. Sun, Energy  
542 saving achieved by limited filamentous bulking sludge under low dissolved oxygen,  
543 *Bioresour. Technol.* 101 (4) (2010) 1120–1126. [https://doi.org/10.1016/j.](https://doi.org/10.1016/j.biortech.2009.09.051)  
544 [biortech.2009.09.051](https://doi.org/10.1016/j.biortech.2009.09.051).

545 [31] S. Lavrnić, S. Cristino, M. Zapater-Pereyra, J. Vymazal, D. Cupido, G. Lucchese, B.  
546 Mancini M.L. Mancini, Effect of earthworms and plants on the efficiency of vertical flow

547 systems treating university wastewater, *Environ. Sci. Pollut. Res.* 26(10) (2019) 10354-  
 548 10362. <https://doi.org/10.1007/s11356-019-04508-4>.

549 [32] M. Li, P. Perez-Calleja, B. Kim, C. Picioreanu, R. Nerenberg, Unique stratification of  
 550 biofilm density in heterotrophic membrane-aerated biofilms: an experimental and modeling  
 551 study. *Chemosphere.* 327 (2023) 138501. [https://doi.org/](https://doi.org/10.1016/j.chemosphere.2023.138501)  
 552 10.1016/j.chemosphere.2023.138501.

553 [33] Y. Wang, M.Y. Xing, J. Yang, B. Lu, Addressing the role of earthworms in treating  
 554 domestic wastewater by analyzing biofilm modification through chemical and spectroscopic  
 555 methods, *Environ. Sci. Pollut. Res.* 23(5) (2016) 4768-4777. [https://doi.org/10.1007/s11356-](https://doi.org/10.1007/s11356-015-5661-6)  
 556 015-5661-6.

557 [34] T. Kumar, K.S. Hari Prasad, N.K. Singh, Substrate removal kinetics and performance  
 558 assessment of a vermifilter bioreactor under organic shock load conditions, *Water Sci.*  
 559 *Technol.* 74(5) (2016) 1177-1184. <https://doi.org/10.2166/wst.2016.303>.

560 [35] S. Ghasemi, M. Mirzaie, A. Hasan-Zadeh, M. Ashrafnejad, S.J. Hashemian, S.R.  
 561 Shahnemati, Design, operation, performance evaluation and mathematical optimization of a  
 562 vermifiltration pilot plan for domestic wastewater treatment. *J. Environ. Chem. Eng.* 8(1)  
 563 (2020) 103587. <https://doi.org/10.1016/j.jece.2019.103587>.

564 [36] A. Rodríguez-Sánchez, J.C. Leyva-Díaz, J.M. Poyatos, J. González-López, Jesús.  
 565 Performance and kinetics of membrane and hybrid moving bed biofilm-membrane  
 566 bioreactors treating salinity wastewater, *AIChE Journal* 63 (2017) 3329-3342.  
 567 <http://doi.org/10.1002/aic.15694>.

568 [37] R. Singh, M. D'Alessio, Jahangeer, Y. Meneses, S. Bartelt-Hunt, C. Ray, Nitrogen  
 569 removal in vermifiltration: mechanisms, influencing factors, and future research needs. *J.*  
 570 *Environ. Manage.* 281 (2021) 111868. <https://doi.org/10.1016/j.jenvman.2020.111868>.

571 [38] S. Arora, S. Saraswat, R. Mishra, J. Rajvanshi, J. Sethi, A. Verma, A. Nag, S. Saxena,  
 572 Design, performance evaluation and investigation of the dynamic mechanisms of earthworm-  
 573 microorganisms interactions for wastewater treatment through vermifiltration technology.  
 574 *Bioresour. Technol.* 12 (2020) 100603. <https://doi.org/10.1016/j.biteb.2020.100603>.

575 [39] S.D. Chowdhury, P. Bhunia, Simultaneous carbon and nitrogen removal from domestic  
 576 wastewater using high rate vermifilter, *Indian J. Microbiol.* 61(2) (2021) 218-228.  
 577 <https://doi.org/10.1007/s12088-021-00936-4>.

578 [40] N. Lourenço, L.M. Nunes, Is filter packing important in a small-scale vermifiltration  
 579 process of urban wastewater? *Int. J. Environ. Sci. Technol.* 14 (11) (2017) 2411-2422.  
 580 <https://doi.org/10.1007/s13762-017-1323-1>.

581 [41] J.J. Elser, K. Acharya, M. Kyle, J. Cotner, W. Makino, T. Markow, T. Watts, S. Hobbie,  
 582 W. Fagan, J. Schade, Growth rate– stoichiometry couplings in diverse biota, *Ecol. Lett.* 6  
 583 (2003) 936-943. <https://doi.org/10.1046/j.1461-0248.2003.00518.x>.

584 [42] X. Wang, J. Bai, Y. Tian, T. Wang, X. Zhou, C. Zhang, Synergistic effects of natural  
 585 ventilation and animal disturbance on oxygen transfer, pollutants removal and microbial  
 586 activity in constructed wetlands, *Chem.* 283 (2021) 131175. <https://doi.org/10.1016/j.chemosphere.2021.131175> .

588 [43] Y. Cao, C. Zhang, H. Rong, G. Zheng, L. Zhao, The effect of dissolved oxygen  
 589 concentration (DO) on oxygen diffusion and bacterial community structure in moving bed  
 590 sequencing batch reactor (MBSBR), *Water Res.* 108 (2017) 86-94.  
 591 <https://doi.org/10.1016/j.watres.2016.10.063>

592 [44] X. Li, M. Xing, J. Yang, Y. Lu, Properties of biofilm in a vermifiltration system for  
 593 domestic wastewater sludge stabilization, *J. Chem. Eng.* 223 (2013) 932-943.  
 594 <https://doi.org/10.1016/j.cej.2013.01.092>.

595 [45] G.U. Semblante, F.I. Hai, H.H. Ngo, W. Guo, S.J. You, W.E. Price, L.D. Nghiem,  
 596 Sludge cycling between aerobic, anoxic and anaerobic regimes to reduce sludge production  
 597 during wastewater treatment: performance, mechanisms, and implications, *Bioresour.*  
 598 *Technol.* 155 (2014) 395–409. <https://doi.org/10.1016/j.biortech.2014.01.029>.

599 [46] J. Tejedor, V. Córdor, C.E. Almeida-Naranjo, V.H. Guerrero, C.A. Villamar,  
 600 Performance of wood chips/peanut shells biofilters used to remove organic matter from  
 601 domestic wastewater. *Sci. Total Environ.* 738 (2020) 139589.  
 602 <https://doi.org/10.1016/j.scitotenv.2020.139589>.

- [47] T. Kumar, R. Bhargava, K.H. Prasad, V. Pruthi, Evaluation of vermifiltration process using natural ingredients for effective wastewater treatment, *Ecol. Eng.* 75 (2015) 370-377. <https://doi.org/10.1016/j.ecoleng.2014.11.044>.
- [48] R. Singh, P. Bhunia, R.R. Dash, COD removal index — A mechanistic tool for predicting organics removal performance of vermifilters, *Sci. Total. Environ.* 643 (2018) 1652-1659. <https://doi.org/10.1016/j.scitotenv.2018.07.272>.
- [49] C. Furlong, W.T. Gibson, A. Oak, G. Thakar, M. Kodgire, R. Patankar, Technical and user evaluation of a novel worm-based, on-site sanitation system in rural India, *Waterlines.* 35 (2016) 148-162. <https://doi.org/10.3362/1756-3488.2016.013>.
- [50] S. Arora, A.A. Kazmi, The effect of seasonal temperature on pathogen removal efficacy of vermifilter for wastewater treatment, *Water Res.* 74 (2015) 88-99. <https://doi.org/10.1016/j.watres.2015.02.001>.
- [51] A.M. Leiva, B. Piña, G. Vidal, Antibiotic resistance dissemination in wastewater treatment plants: a challenge for the reuse of treated wastewater in agriculture, *Rev. Environ. Sci. Biotechnol.* 20 (2021) 1043–1072. <https://doi.org/10.1007/s11157-021-09588-8>.
- [52] L. Antinolo Bermudez, E.M. Martinez Sanchez, J.C. Leyva Diaz, M. D. M. Munio Martinez, J. M. Poyatos Capilla, J. Martin Pascual, Impacts of Organic Emerging Contaminants (Erythromycin, Ibuprofen, and Diclofenac) on the Performance of a Membrane Bioreactor Treating Urban Wastewater: A Heterotrophic Kinetic Investigation. *Membranes.* 13 (2023). <https://doi.org/10.3390/membranes13080697>.
- [53] Z.L. Wei, Miao, J., Z.W. Yang, D.Y. Shi, H.Y.Wu, D. Yang, M.Jin, Contamination sources of the enteric virus in recreational marine water shift in a seasonal pattern. *Sci. Total Environ.* 743 (2020) 140641. <https://doi.org/10.1016/j.scitotenv.2020.140641>.
- [54] C. Di Iaconi, M. De Sanctis, A. Lopez, A single-stage biological process for municipal sewage treatment in tourist areas. *J. Environ. Manage.* 144 (2014) 34-41. <https://doi.org/10.1016/j.jenvman.2014.05.008>
- [55] A. Kumar, M. Khwairakpam, 2024. A comparative study with vermifilter and geofilter for domestic wastewater treatment and its Phyto-toxicity efficacy, *JWPE.* 60 (2024) 105245. <https://doi.org/10.1016/j.jwpe.2024.105245>

632 [56] R. Singh, P. Bhunia, R.R. Dash, Impact of Organic Loading Rate and Earthworms on  
633 Dissolved Oxygen and Vermifiltration, *J. Hazard. Toxic Radioact. Waste.* 23 (2019)  
634 4019001. [https://doi.org/ 10.1061/\(ASCE\)HZ.2153-5515.000043](https://doi.org/10.1061/(ASCE)HZ.2153-5515.000043).

635 [57] R. Singh, P. Bhunia, R.R. Dash, A mechanistic review on vermifiltration of wastewater:  
636 design, operation and performance. *J. Environ. Manage.* 197 (2017) 656-672.  
637 <https://doi.org/10.1016/j.jenvman.2017.04.042>.

638 [58] L. Wang, X. Luo, Y. Zhang, J. Chao, Y. Gao, J. Zhang, Z. Zheng, Community analysis  
639 of ammonia-oxidizing Betaproteobacteria at different seasons in microbial-earthworm  
640 ecofilters, *Ecol. Eng.* 51 (2013) 1–9. [https://doi.org/ 10.1016/j.ecoleng.2012.12.062](https://doi.org/10.1016/j.ecoleng.2012.12.062).

641 [59] R.K. Sinha, G. Bharambe, U. Chaudhari, Sewage treatment by vermifiltration with  
642 synchronous treatment of sludge by earthworms: a low-cost sustainable technology over  
643 conventional systems with potential for decentralization, *Environmentalist.* 28 (4) (2008)  
644 409–420. <https://doi.org/10.1007/s10669-008-9162-8>.

645 [60] O. Bajsa, J. Nair, K. Mathew, G.E. Ho, Vermiculture as a tool for domestic wastewater  
646 management, *Water. Sci. Technol.* 48 (2003), 125–132.  
647 <https://doi.org/10.2166/wst.2004.0821>.

648 [61] S. Arora, A.A. Kazmi, Reactor performance and pathogen removal during wastewater  
649 treatment by vermifiltration, *J Water Sanit Hyg Dev.* 6 (2016) 65-73.  
650 <https://doi.org/10.1016/j.watres.2015.02.001>.

651 [62] K. Samal, R.R Dash, P. Bhunia, Treatment of wastewater by vermifiltration integrated  
652 with macrophyte filter: A review. *J. Environ. Chem. Eng.* 5 (2017) 2274-2289.  
653 <https://doi.org/10.1016/j.jece.2017.04.026>.

654 [63] R. Singh, K. Samal, R.R Dash, P. Bhunia, Vermifiltration as a sustainable natural  
655 treatment technology for the treatment and reuse of wastewater: A review, *J. Environ.*  
656 *Manage.* 247 (2019) 140-151. <https://doi.org/10.1016/j.jenvman.2019.06.075>.

657 [64] P. Andreo-Martínez, N. García-Martínez, J. Quesada-Medina, L. Almela, Domestic  
658 wastewaters reuse reclaimed by an improved horizontal subsurface-flow constructed  
659 wetland: a case study in the southeast of Spain. *Bioresour Technol.* 233 (2017) 236–246.  
660 <https://doi.org/10.1016/j.biortech.2017.02.123>

[65] W. Huang, Y. Zhao, J. Wu, J. Zhang, Z. Zheng, Effects of different influent C/N ratios on the performance of various earthworm eco-filter systems: nutrient removal and greenhouse gas emission, *World J. Microbiol. Biotechnol.* 30 (1) (2014) 109-118. <https://doi.org/10.1007/s11274-013-1430-1>.

[66] E. Ranieri, G. D' Onghia, L. Lopopolo, P. Gikas, F. Ranieri, E. Gika, V. Spagnolo, A.C. Ranieri, Evaluation of greenhouse gas emissions from aerobic and anaerobic wastewater treatment plants in Southeast of Italy, *J. Environ. Manag.* 337 (2023) 117767. <https://doi.org/10.1016/j.jenvman.2023.117767>.

687

688

### Table Captions

689 **Table 1.** Summary of design and operating parameters of the vermifilter.

690 **Table 2.** Key kinetic parameters of the respirometry test.

691 **Table 3.** Kinetic parameters of heterotrophic biomasses in different WWTPs.

692 **Table 4.** Kinetic parameters of the heterotrophic biomass in a VF between seasons.

693

694

695

696

697

698

699

700

701

702

703

704

705

706

707

708

709

710

711

| Parameter                | Unit                             | Value                  |
|--------------------------|----------------------------------|------------------------|
| Volume                   | m <sup>3</sup>                   | 442                    |
| Area                     | m <sup>2</sup>                   | 276                    |
| Height                   | m                                | 1.60                   |
| Influent flow            | m <sup>3</sup> /d                | 160                    |
| HLR                      | m <sup>3</sup> /m <sup>2</sup> d | 0.60                   |
| Influent COD             | kg COD                           | 0.89                   |
| OLR                      | kg COD/m <sup>2</sup> d          | 0.54                   |
| Carbon/nitrogen ratio    | -                                | 9                      |
| Active layer             | -                                | Wood chips             |
| Active layer height      | m                                | 0.92 ± 0.12            |
| Active layer volume      | m <sup>3</sup>                   | 254                    |
| Species                  | -                                | <i>Eisenia foetida</i> |
| Earthworm density Zone A | worm/m <sup>3</sup>              | 1105 ± 982             |
| Earthworm density Zone B | worm/m <sup>3</sup>              | 7221 ± 1699            |

712 **Note:** HLR: hydraulic loading rate; OLR: organic loading rate; COD: chemical oxygen  
713 demand.

714 **Table 1**

715

716

717

718

719

720

721

722

723

| kinetic parameters                           | Unit              | Equation                              | Description                                       |
|----------------------------------------------|-------------------|---------------------------------------|---------------------------------------------------|
| Oxygen uptake rate ( $OUR_{end}$ )           | $mgO_2/L \cdot h$ | $\Delta OC/\Delta t$                  | Oxygen consumption rate                           |
| Specific oxygen uptake rate ( $SOUR_{end}$ ) | $mgO_2/gVSSh$     | $OUR/VSS$                             | Oxygen consumption rate of active biomass         |
| Heterotrophic biomass yield ( $Y_H$ )        | $mgCODm/mgCODs$   | $1 - \Delta OC/COD$                   | Biomass generated per unit of exogenous substrate |
| Endogenous decay constant ( $K_d$ )          | $d^{-1}$          | $SOUR_{end}/1.48$                     | Mortality constant of heterotrophic biomass       |
| $\mu_H$                                      | $d^{-1}$          | $Y_{hvss} \cdot 24 \cdot (U/X) - K_d$ | Heterotrophic biomass growth rate                 |
| $\mu_{max}$                                  | $d^{-1}$          | $\mu_H \cdot (K_s + S)/S$             | Maximum heterotrophic biomass growth rate         |

**Note:** Fcv: 1.48. Stoichiometric adjustment factor for reactions involved in the organic matter degradation process [10]; U: Substrate use rate (mgCODs/h);  $X_H$ : Active heterotrophic biomass; CODm: COD of microorganisms generated; CODs: COD of the substrate consumed;  $K_s$ : Semi – Saturation constant; S: COD removed.

**Table 2**

| Type      | OUR <sub>end</sub><br>(mgO <sub>2</sub> /L·h) | SOUR <sub>end</sub><br>(mgO <sub>2</sub> /gVSSh) | Y <sub>H</sub><br>(mgCOD <sub>m</sub> /mgCOD <sub>s</sub> ) | μ <sub>max</sub><br>(d <sup>-1</sup> ) | K <sub>d</sub><br>(d <sup>-1</sup> ) | References |
|-----------|-----------------------------------------------|--------------------------------------------------|-------------------------------------------------------------|----------------------------------------|--------------------------------------|------------|
| UCT-MBR   | 2-6                                           | -                                                | 0.57-0.74                                                   | 0.40-2.40                              | 0.26*                                | [28]       |
| IFAS-MBR  | -                                             | -                                                | 0.64                                                        | 8.99                                   | 0.19*                                | [29]       |
| IFAS-MBR  |                                               |                                                  | 0.66                                                        | 3.66                                   | 0.24*                                | [29]       |
| CAS       | -                                             | -                                                | 0.67                                                        | 6.0                                    | 0.21*                                | [16]       |
| OSA       | -                                             | -                                                | 0.67                                                        | 6.0                                    | 0.32*                                | [16]       |
| UASB-MBR  | 1.55                                          | 1.49                                             | 0.71*                                                       | -                                      | 0.03                                 | [10]       |
| UASB-MBRs | 2.20                                          | 1.15                                             | 0.41*                                                       | -                                      | 0.02                                 | [10]       |
| CAS       | 3.60-15.30                                    | 0.9-4.0                                          | 0.86                                                        | 2.28-3.00                              | 0.06                                 | [19]       |
| CAS       | 0.053                                         | -                                                | 0.23                                                        | 0.17                                   | 0.01                                 | [15]       |
| CAS       | 1.76-2.28                                     | -                                                | 0.73*                                                       | 0.047                                  | 1.45*                                | [20]       |
| VF        | 1.22                                          | 1.24                                             | 0.47                                                        | 0.05                                   | 0.03                                 | This study |

**Note:** UCT: Anaerobic-anoxic-aerobic. MBR: Membrane bioreactors. MBRs: Membrane bioreactors with supported biomass. IFAS: Integrated fixed film activated sludge. CAS: Conventional activated sludge. OSA: Oxidic settling anoxic. UASB: Upflow anaerobic sludge blanket. VF: Vermifilter. OUR: Oxygen uptake rate. SOUR: Specific oxygen uptake rate. VSS: Volatile suspended solids. COD<sub>m</sub>: COD of microorganisms generated; COD<sub>s</sub>: COD of the substrate consumed. \* Y<sub>H</sub> was calculated with fcv= 1.48. Stoichiometric adjustment factor for reactions involved in the organic matter degradation process [10]; \*K<sub>d</sub> was calculated with the decay rate b<sub>H</sub>.

**Table 3**

| Parameter           | Unity           | Fall-Winter | Spring-Summer |
|---------------------|-----------------|-------------|---------------|
| OUR <sub>end</sub>  | mg/L·h          | 1.15        | 2.25          |
| SOUR <sub>end</sub> | mg/gVSSh        | 1.05        | 2.25          |
| Y <sub>H</sub>      | mgCODm/ mgCODs  | 0.39        | 0.54          |
| μ <sub>max</sub>    | d <sup>-1</sup> | 0.07        | 0.02          |
| K <sub>d</sub>      | d <sup>-1</sup> | 0.02        | 0.04          |

**Note.** OUR: Oxygen uptake rate. SOUR: Specific oxygen uptake rate. VSS: Volatile suspended solids. CODm: COD of microorganisms generated; CODs: COD of the substrate consumed.

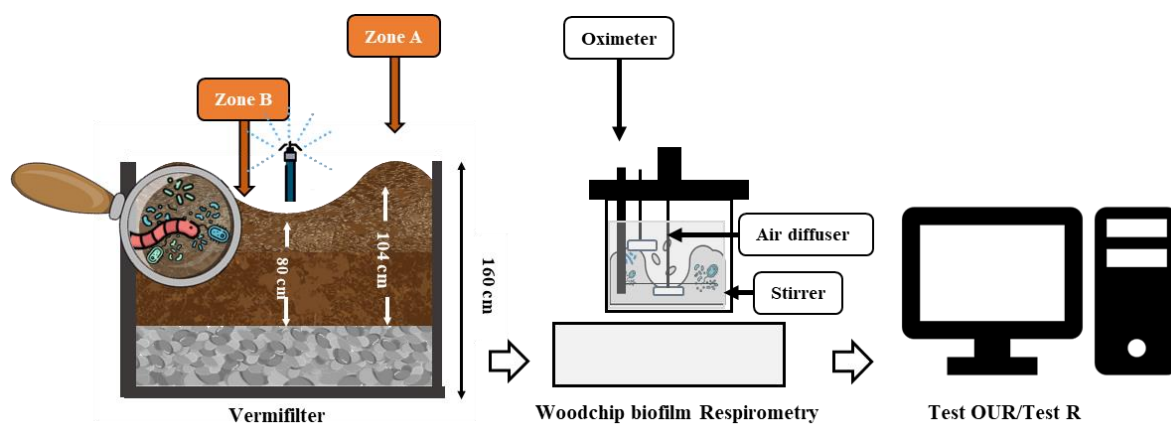
**Table 4**

### Figure captions

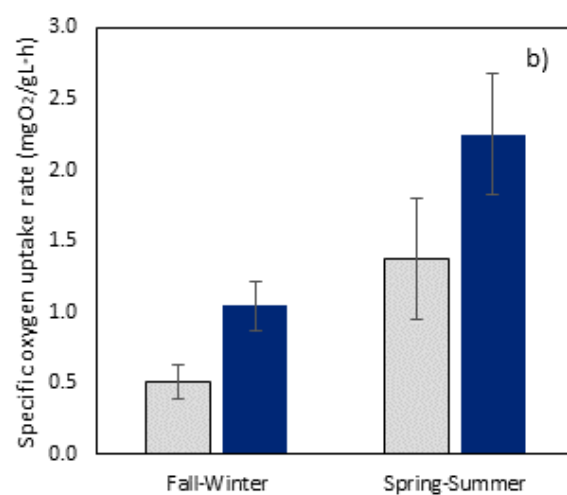
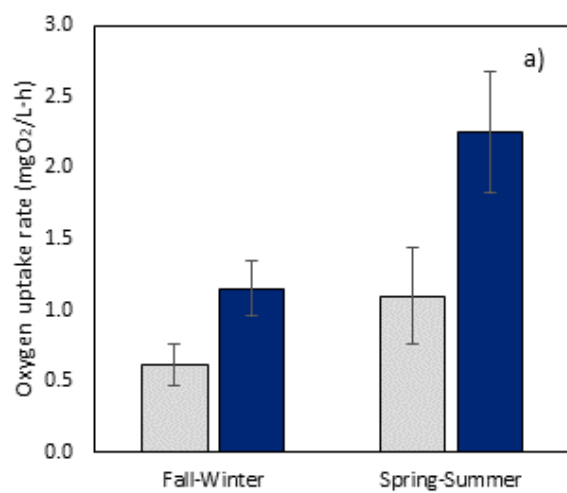
**Figure 1.** Schematic representation of a VF and respirometry test.

**Figure 2.** Respirometry test in different seasons and with different earthworm densities. a)  $OUR_{end}$  and b)  $SOUR_{end}$ . Where  Zone A:  $1105 \pm 982$  worms/m<sup>3</sup>;  Zone B:  $7221 \pm 1699$  worms/m<sup>3</sup>.

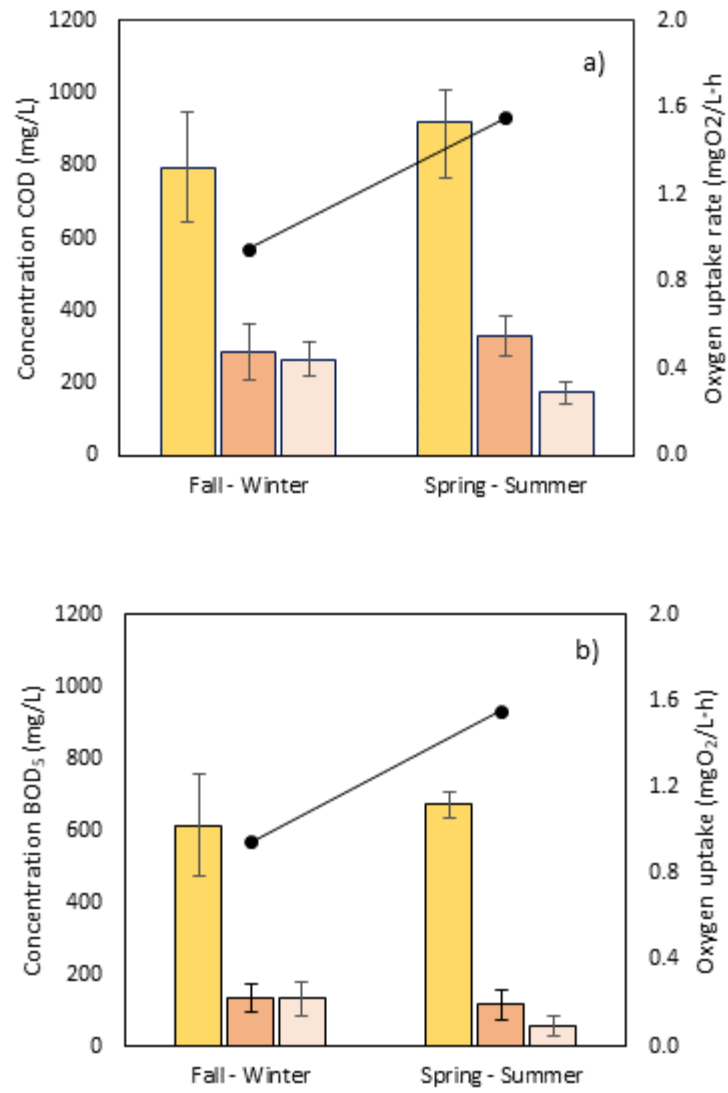
**Figure 3.** Concentrations (mg/L) of a) COD and b)  $BOD_5$  in IN () , E1 () , and E2 () and  $OUR_{end}$  in fall-winter and spring-summer



**Figure 1**



**Figure 2**



**Figure 3**